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# Hybrid photothermal–photocatalyst sheets for solar-driven overall water splitting coupled to water purification

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### Supplementary Discussion 1 | Justification for materials selection for sheet fabrication.

Aluminium-doped strontium titanate (Al:SrTiO<sub>3</sub>) was selected as a UV-active PC material due to its high activity toward overall water splitting, simple synthesis and low cost.<sup>1,2</sup> Depending on the co-catalyst and loading method, Al:SrTiO<sub>3</sub> can yield overall water splitting with an external quantum efficiency of 68-98% at 350 nm.<sup>3,4</sup> The impregnation technique was utilized for co-catalyst deposition instead of photodeposition, which would provide a higher activity, due to its potential for scalability.<sup>5</sup> The trade-off of this simple fabrication procedure is the inherently lower efficiency of the photocatalyst. The carbon-based gas diffusion layer consisting of a fibrous macroporous bottom layer and a smooth macroporous top layer (Fig. 2c, Supplementary Fig. 3) was selected as the SVG due to three reasons: (i) the light-weight substrate (density  $\approx 0.49 \text{ g cm}^{-3}$ ) is able to float on the liquid surface, (ii) the porous structure of the bottom surface facilitates efficient water transport and (iii) the black colour and light-scattering nature of the top macroporous surface allows for broad-spectrum solar absorption to generate heat (Fig. 1e), while being small enough for deposition of the PC layer.

### Supplementary Discussion 2 | Photocatalyst loading optimization.

To investigate the optimum PC powder loading, the photothermal-photocatalyst sheets (photoactive area:  $1 \times 1 \text{ cm}^2$ ) with 0.5–4.0  $\text{mg cm}^{-2}$  of RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> loading were first prepared and tested on Milli-Q water. The photographs and SEM images show different extent of PC coverage and thickness on the SVG ranging from 1–10  $\mu\text{m}$  (Supplementary Figs. 25–27). Fig. 2d shows that the H<sub>2</sub> produced (per irradiated area) and the solar-to-H<sub>2</sub> (STH) efficiency increases with PC loading and starts to saturate beyond a loading of 2.0  $\text{mg cm}^{-2}$ . The highest H<sub>2</sub> evolution rate of  $20.6 \pm 3.7 \text{ mmol m}^{-2} \text{ h}^{-1}$  (corresponding to an STH efficiency of  $0.13 \pm 0.02\%$ ) was obtained with a catalyst loading of 4.0  $\text{mg cm}^{-2}$ . The H<sub>2</sub> produced (per gram catalyst) remains constant up to 2.0  $\text{mg PC cm}^{-2}$  and then starts to decrease significantly due to light shielding by the excess photocatalyst layer formed at high catalyst loadings. (Supplementary Table 16).

Vapour generation was studied in a custom  $1.5 \times 1.5 \times 5.0 \text{ cm}^3$  reactor with an open top (Supplementary Fig. 24). While the bare SVG substrate had a vapour generation rate of  $1.07 \pm 0.08 \text{ kg m}^{-2} \text{ h}^{-1}$  (compared to a base rate of  $0.55 \pm 0.11 \text{ kg m}^{-2} \text{ h}^{-1}$  without SVG), the rates obtained by the photothermal-photocatalyst sheets with 0.0–4.0  $\text{mg cm}^{-2}$  PC generally decreased from  $1.07 \pm 0.08$  to  $0.88 \pm 0.15 \text{ kg m}^{-2} \text{ h}^{-1}$ , corresponding to a drop in solar thermal conversion efficiency ( $\eta$ ) from  $67.7 \pm 5.2$  to  $55.3 \pm 9.4\%$ , which agrees well with reported literature values for carbonaceous SVG (Fig. 2e, Supplementary Tables 3). A slight decreasing trend was observed with increasing catalyst loading due to light blocking and scattering by the PC top layer, which suggests that excessive PC loading can negatively impact the SVG performance.

Based on the above results, a trade-off is necessary to balance PC cost, vapour generation rate and overall device activity. A lower catalyst loading allows for material saving and better vapour transport through the PC layer, whereas a higher catalyst loading may enable better thermal insulation and reduce heat losses, at the cost of increasing vapour transport resistance and reducing visible and IR light transmittance. Taking these factors into account, an optimal catalyst loading of 2.0 mg was selected and used in all subsequent experiments. This was primarily due the drop in photocatalytic productivity as indicated by the decrease in H<sub>2</sub> evolution per gram catalyst beyond a catalyst loading of 2.0 mg (Fig. 2d). From an economic standpoint, catalyst loadings above 2.0 mg yield diminishing returns as the cost of additional PC material outweighs the relatively small increase in product H<sub>2</sub>. On the other hand, while catalyst loading also affects the vapour generation rate of the PC sheets, this factor was less important as there was only a marginal decrease in vapour generation rate with increasing catalyst loading (Fig. 2e). Furthermore, at all catalyst loadings, the vapour generation rate was well over the water utilization rate by photocatalysis, meaning that the supply of feedstock to the PC layer was not a significant element to consider.

### **Supplementary Discussion 3 | Performance of SVG-PC versus Glass-PC.**

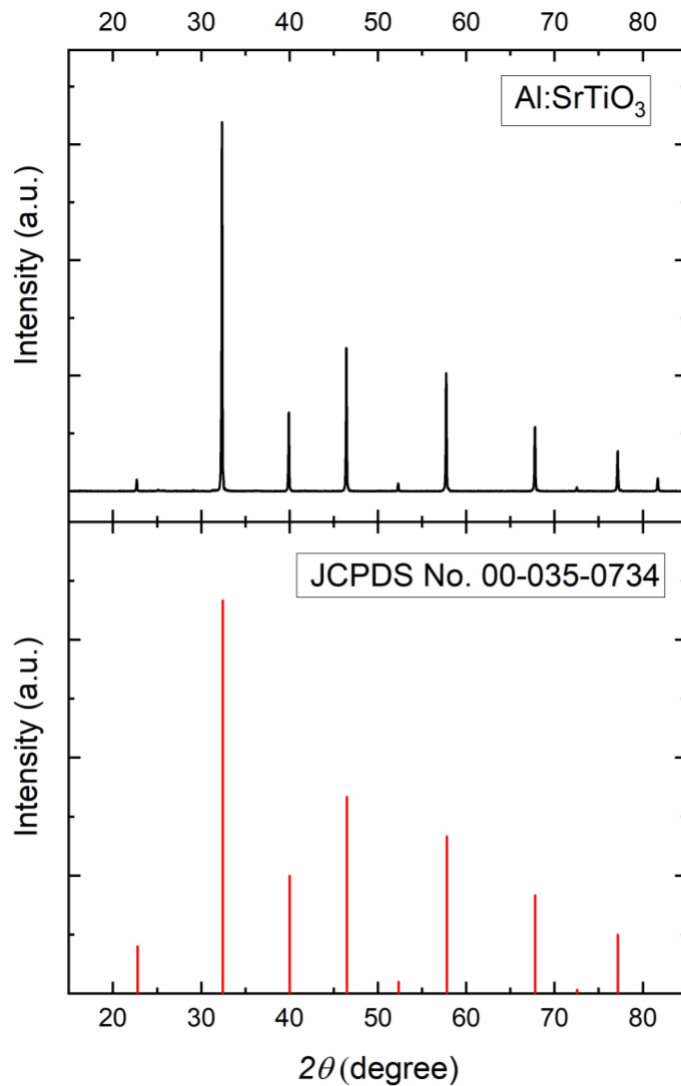
While our SVG-PC system outperformed untreated SVG-PC and Glass-PC (liquid-phase) for seawater splitting, it displayed a ~20% lower H<sub>2</sub> evolution rate than Glass-PC in pure water (Fig. 3a). The reason for the lower activity in vapour-phase water splitting is attributed to the lower water partial pressure, and limited interaction of vapour and the PC surface,<sup>6</sup> which leads to a lower coverage of water molecules on the surface of the photocatalyst.<sup>7</sup> This drop in performance is relatively small compared to other reported gas-phase water splitting systems which see far more substantial declines in performance when replacing liquid water by water vapour.<sup>7,8</sup> In our current design, the constant flux of water vapour passing through the PC layer might help increase the water molecule coverage, bridging the performance gap between the liquid-and gas-phase water splitting systems. The temperature achieved at the SVG-PC interface may also play an important role in the high activity of our system.

### **Supplementary Discussion 4 | Elaboration on the techno-economic analysis of the floating photocatalyst sheet and particulate photocatalyst water splitting panel systems.**

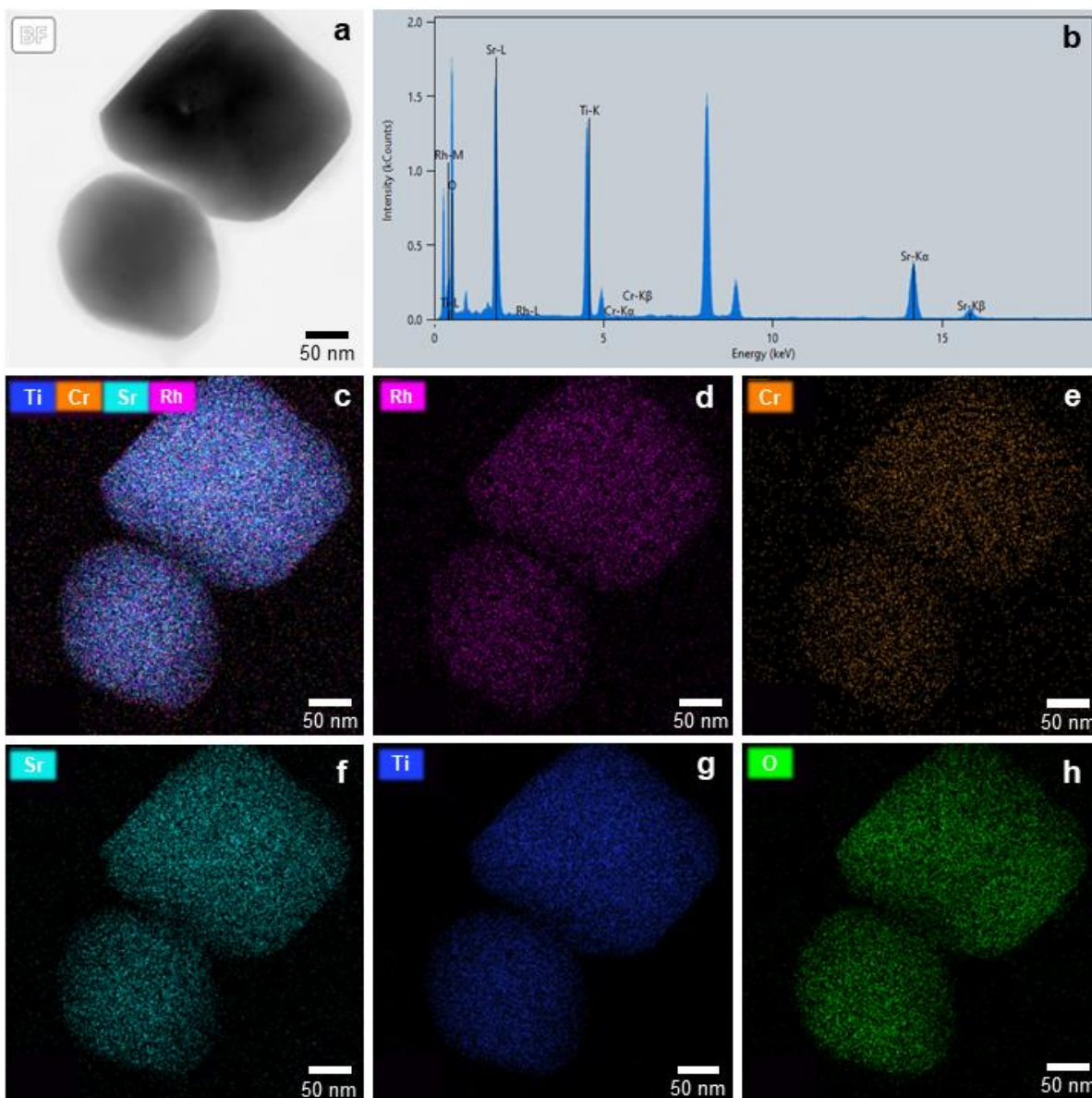
The techno-economic analysis of the hypothetical large-scale solar water splitting systems were based on the floating photocatalyst sheet design introduced in this study and on a previously reported particulate photocatalyst water splitting panel system.<sup>3</sup> The capital and operating costs of the large-scale systems were estimated assuming the general STH target for particulate photocatalytic system of 10%, capacity of 1 tonne per day of H<sub>2</sub>, average solar insolation of 0.24 kW m<sup>-2</sup>, and a facility lifetime of 20 years.<sup>9-11</sup>

The reactor subassemblies of both systems, consisting of a reaction chamber, an illumination window and support frames, are expected to be similar due to the fact that both systems comprise a photocatalyst immobilized on a sheet or panel<sup>12</sup> The costs of auxiliary equipment and control systems for gas handling, as well as the labour and energy required to operate them were estimated by extrapolating data from the economic analyzes of other solar H<sub>2</sub> production plants.<sup>9,13,14</sup> The land and maintenance costs of the two systems were taken as 6% of their equipment cost and total capital cost, respectively. The model particulate photocatalyst chosen for this techno-economic analysis was CoP-modified graphitic carbon nitride due to its scalability and high theoretical STH efficiency.<sup>15-17</sup> For the floating photocatalyst sheet system, the cost of the solar vapour generator was estimated from the current price of a commercially available carbon paper.

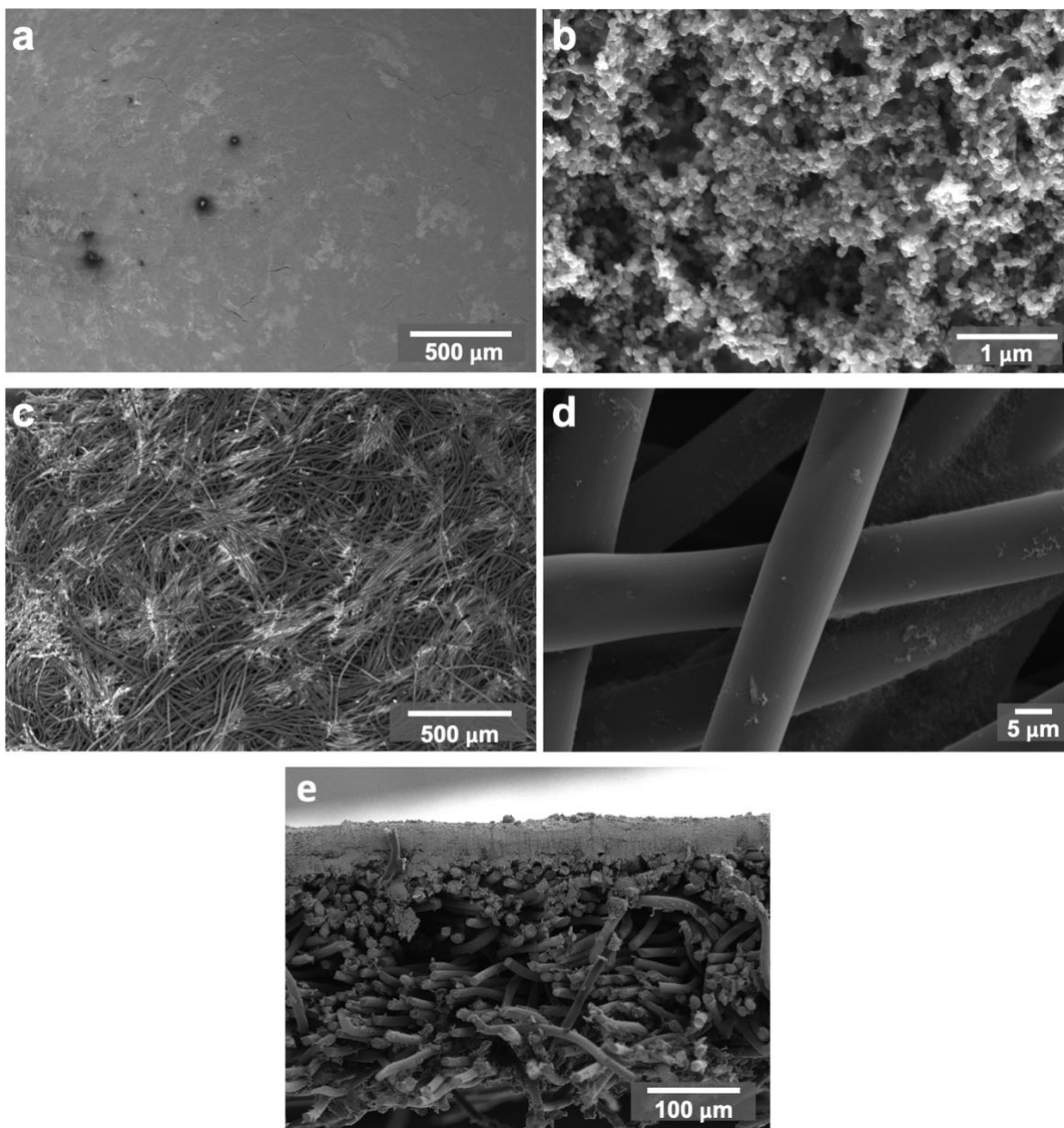
From the analysis (Supplementary Table 15), it can be seen that pure water is estimated to be one of the largest expenditures in a hypothetical large-scale solar water splitting system. Hence, the ability of the floating photocatalyst sheets to utilize contaminated water feedstocks for photocatalysis would significantly increase the economic feasibility of such a system. Operating the floating photocatalyst sheets over open bodies of water will further drive down the cost of this system by reducing the cost of land. In addition, this approach yield distilled water which can then be used by the neighbouring area for agriculture as well as consumption. However, it should be noted that the fabrication cost of the floating photocatalyst sheets is higher than the particulate photocatalyst water splitting panels due to the need for a solar vapour generator and a higher catalyst loading. This could be addressed by utilizing locally sourced carbonized biomass materials such as rice barn for the fabrication of the substrate for solar vapour generator.<sup>18</sup>



**Supplementary Figure 1 | X-ray diffraction (XRD) patterns for Al:SrTiO<sub>3</sub>.** XRD peaks of Al:SrTiO<sub>3</sub> match with the standard pattern of SrTiO<sub>3</sub> (PDF No. 00-035-0734) and no other phases were found. XRD data processed using JADE software.

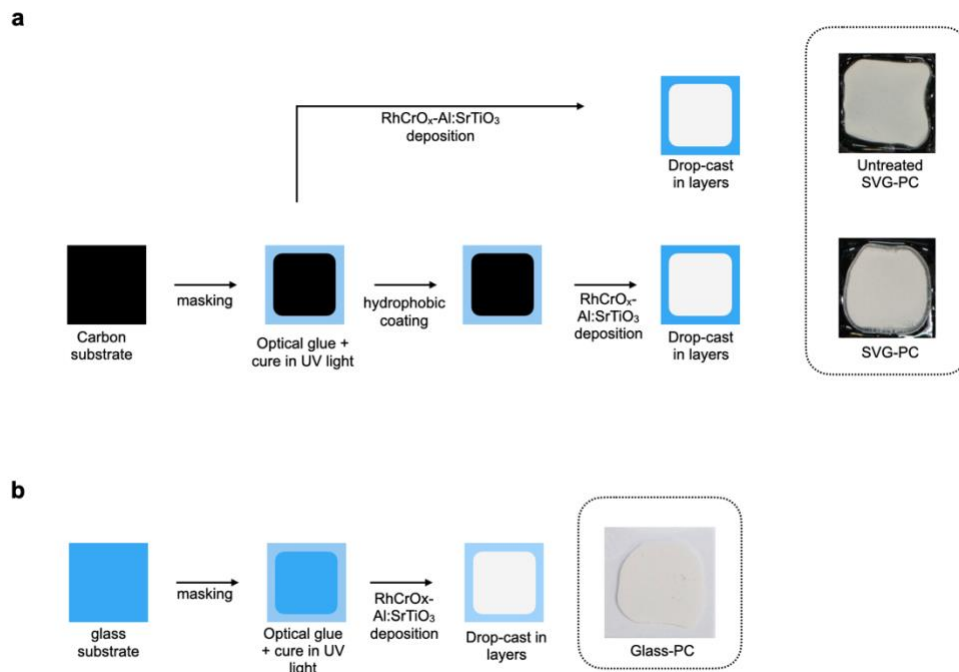


**Supplementary Figure 2 | TEM images and energy-dispersive X-ray (EDX) elemental mapping of as-prepared RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> powder. a, TEM image of RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub>. b, EDX elemental spectrum corresponding to the area depicted in (a). c-h, Overall (c), Rh (d), Cr (e), Sr (f), Ti (g) and O (h) elemental mapping.**

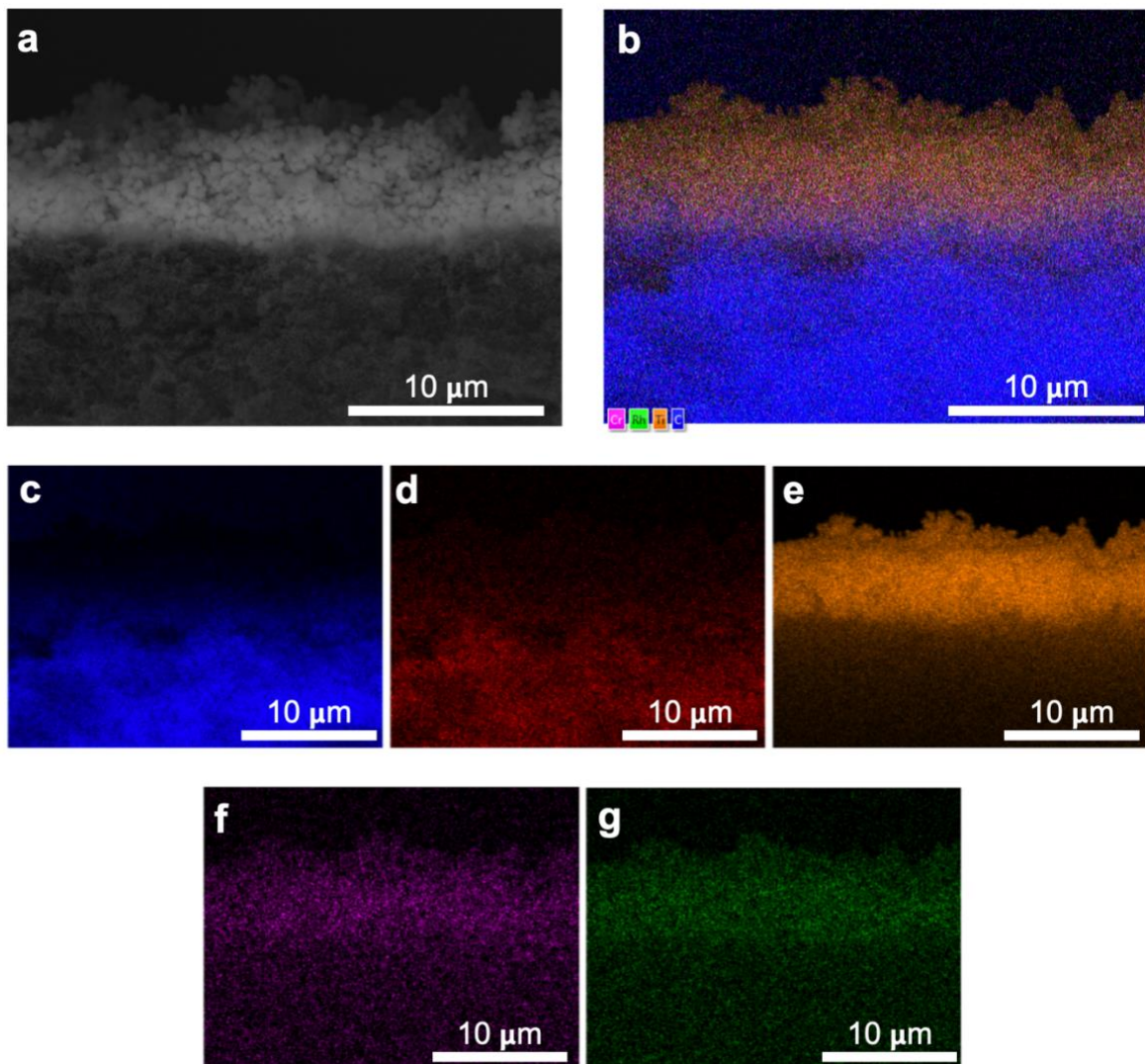


**Supplementary Figure 3 | SEM images of the gas-diffusion carbon paper substrate which functions as an SVG. a, b, Top; c, d, bottom; and e, cross-sectional SEM images of the carbon paper. Mass per area of SVG is  $0.012 \text{ g cm}^{-2}$ .**

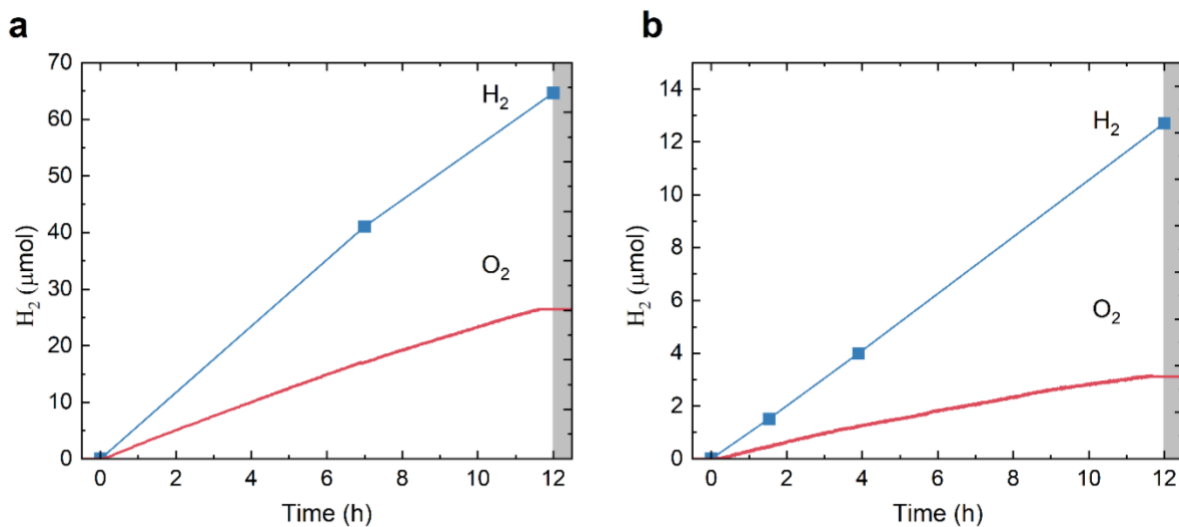




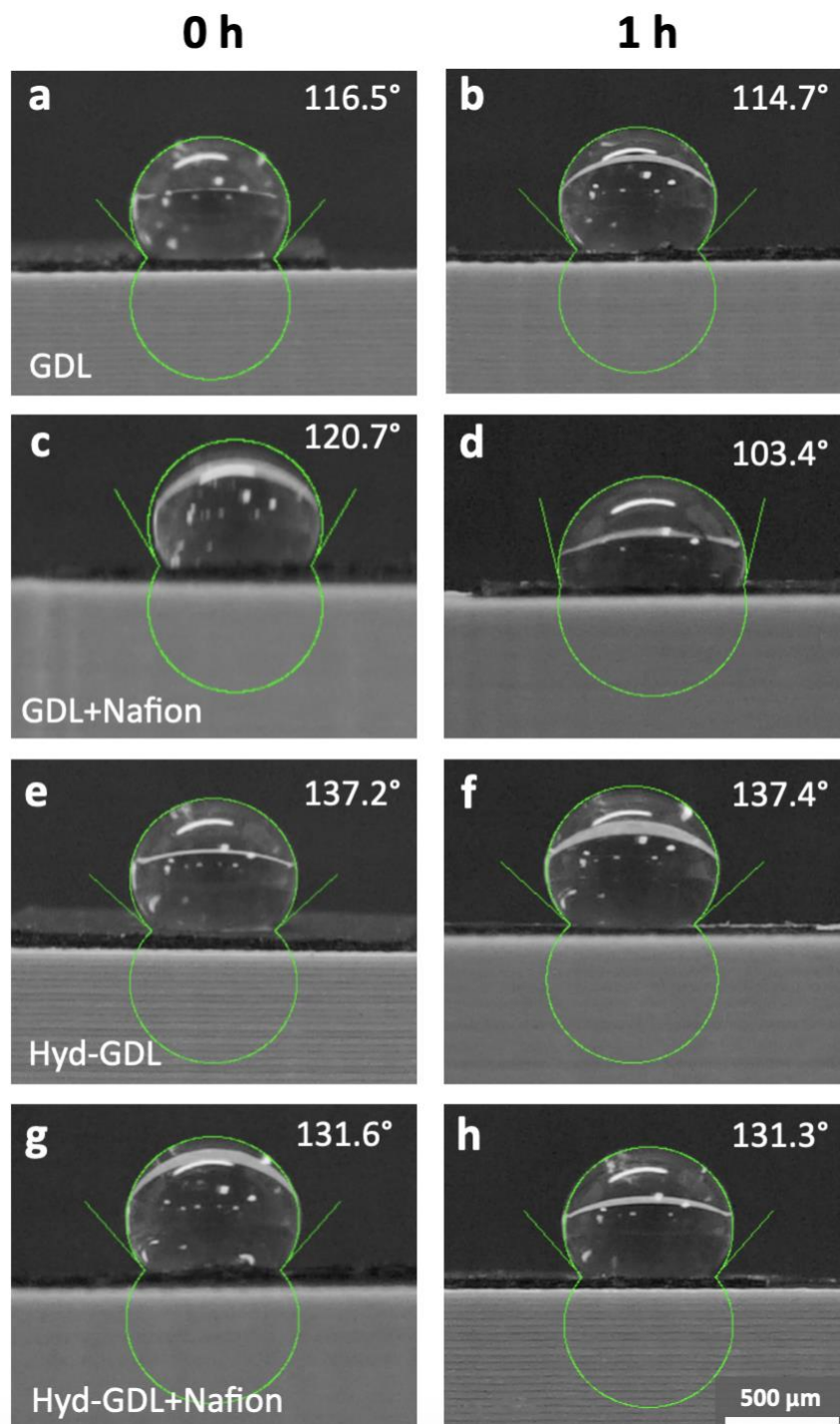
**Supplementary Figure 4 | Step-by-step device assembly. a**, Assembly of SVG-PC. The perimeter of a sheet of carbon paper is masked with optical glue and is hydrophobically-treated with DCDMS solution. Finally, RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> dispersed in IPA is drop-casted onto the sheet with a Nafion top-layer and dried at 338 K overnight. In the case of untreated SVG-PC, the hydrophobic treatment is skipped. **b**, Assembly of Glass-PC. The perimeter of a glass sheet is masked with optical glue. RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> dispersed in IPA is drop-casted onto the sheet. The glue mask was removed and the sheet was annealed at 573K for 1 h.



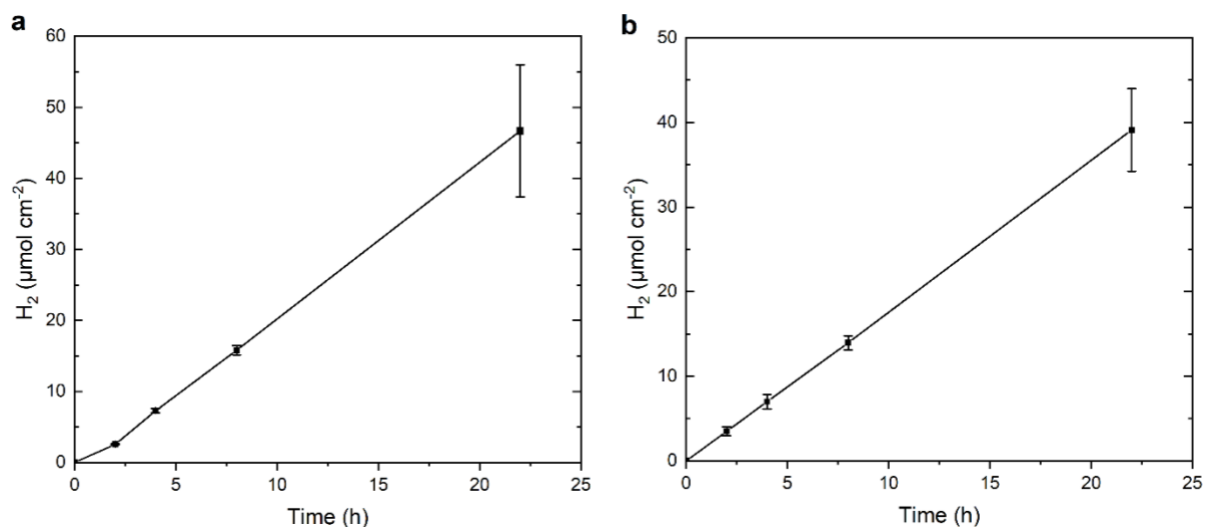
**Supplementary Figure 5 | Cross-section SEM images and energy-dispersive X-ray (EDX) elemental mapping of as-prepared SVG-PC sheet. a**, SEM image recorded at 15.0 kV beam intensity. **b-g**, Overall (**b**), carbon (**c**), fluorine (**d**), titanium (**e**), chromium (**f**) and rhodium (**g**) elemental mapping.



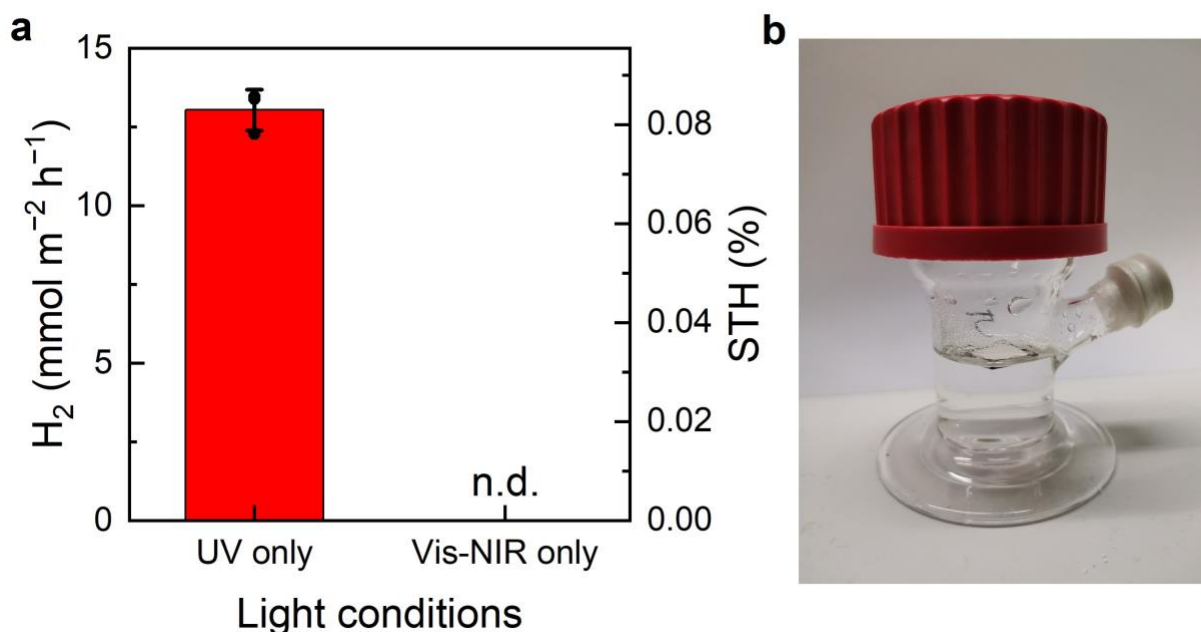
**Supplementary Figure 6 | A typical time course of the water-splitting reaction over a RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> photocatalyst. a, b**, RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> suspension in distilled water (a) and in artificial seawater (b). Photocatalytic measurements were performed under simulated sunlight (AM 1.5G, 100 mW cm<sup>-2</sup>). The grey portion of the graphs indicate when the samples were removed from irradiation, allowing the baseline O<sub>2</sub> to be measured to account for possible O<sub>2</sub> leakage.



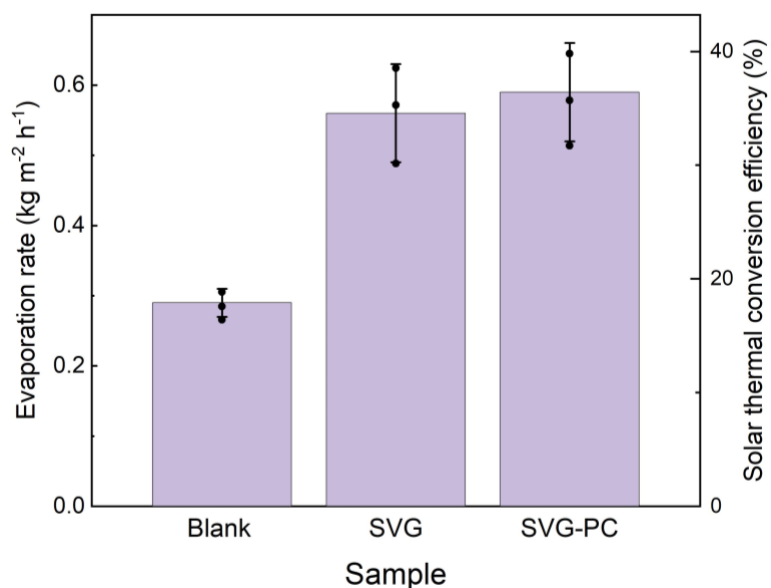
**Supplementary Figure 7 | Contact angle measurement of SVG.** **a, b**, Contact angle of SVG at 0 h (**a**) and 1 h (**b**). **c, d**, Contact angle of Nafion-coated SVG at 0 h (**c**) and 1 h (**d**). **e, f**, Contact angle of hydrophobically-treated SVG at 0 h (**e**) and 1 h (**f**). **g, h**, Contact angle of Nafion-coated on hydrophobically-treated SVG at 0 h (**g**) and 1 h (**h**). To carry out the contact angle measurements, two sets of sheets were floated on pure water; a droplet of water was applied to the first set at 0 h and the second set at 1 h.



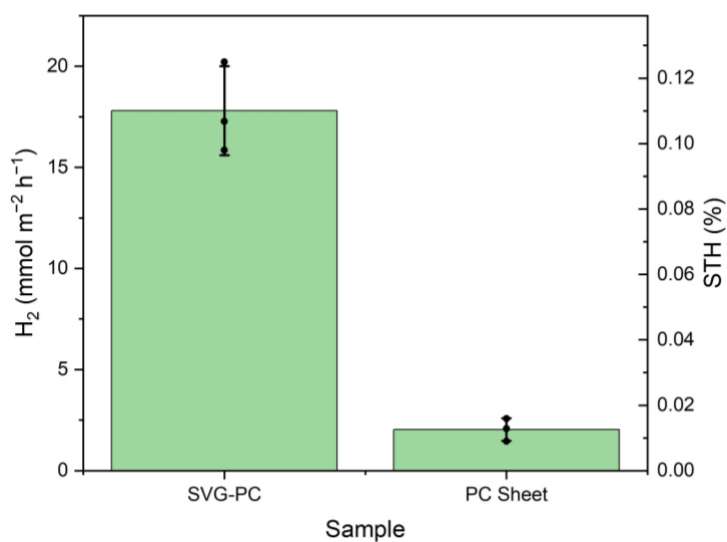
**Supplementary Figure 8 | Sample time course of H<sub>2</sub> evolution using SVG-PC. a-b.** H<sub>2</sub> evolution measurements performed over pure water (a) and seawater (b). Conditions: 2.0 mg RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> deposited on hydrophobic-treated SVG, irradiation (AM 1.5G, 1 sun, 22 h). Data are presented as mean values ± SD with n = 3.



**Supplementary Figure 9 | Photocatalytic experiments conducted under different light conditions. (a)** H<sub>2</sub> evolution rate of SVG-PC under UV and Vis-NIR light. **(b)** Photograph of the photoreactor taken after conducting the photocatalytic experiment under only UV irradiation. Condensation on the walls of the photoreactor indicate that water vapour builds-up in the reactor despite the exclusion of Vis and NIR light. Photocatalytic measurements were performed over pure water for 22h. n.d. – not detected. Reported value can be seen in Supplementary Table 7. Data are presented as mean values ± SD with n = 3.

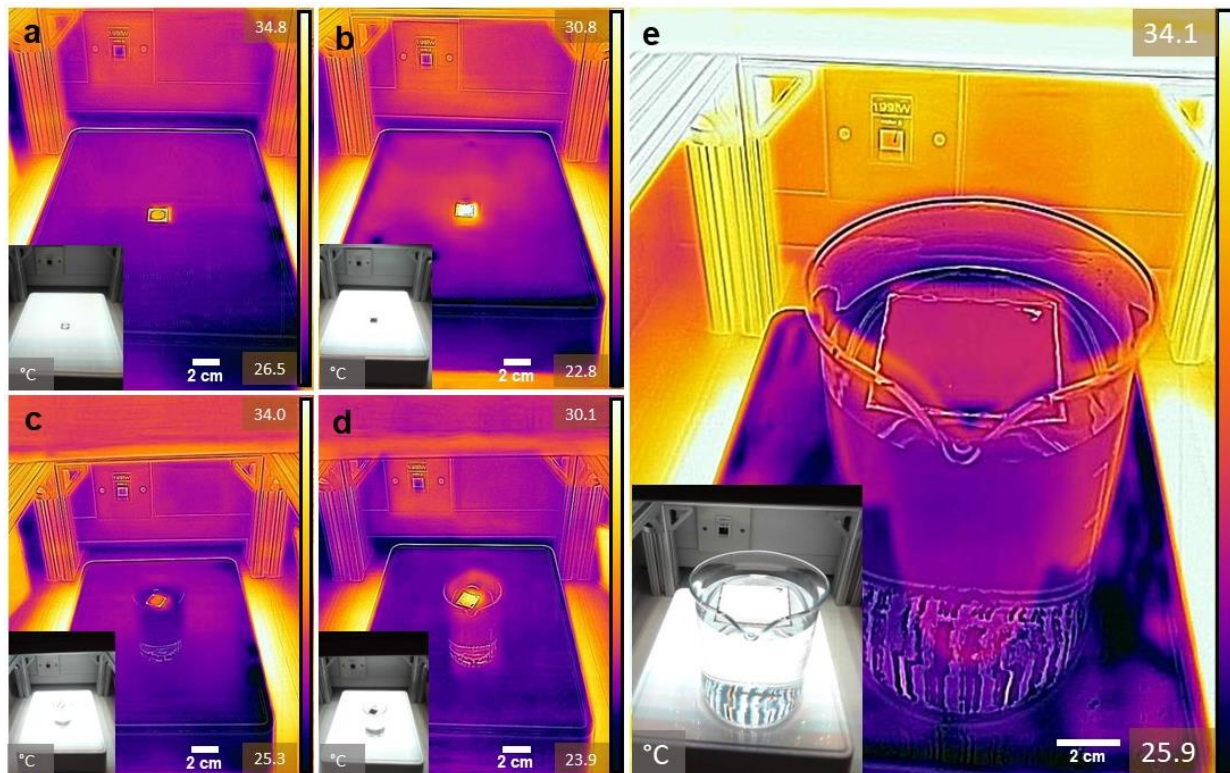


**Supplementary Figure 10 | Solar vapour generation rate for the photothermal-photocatalyst sheets and SVG substrate under UV light irradiation.** Water evaporation measurements were performed using pure water for 4 h, respectively. Data are presented as mean values  $\pm$  SD with  $n = 3$ .

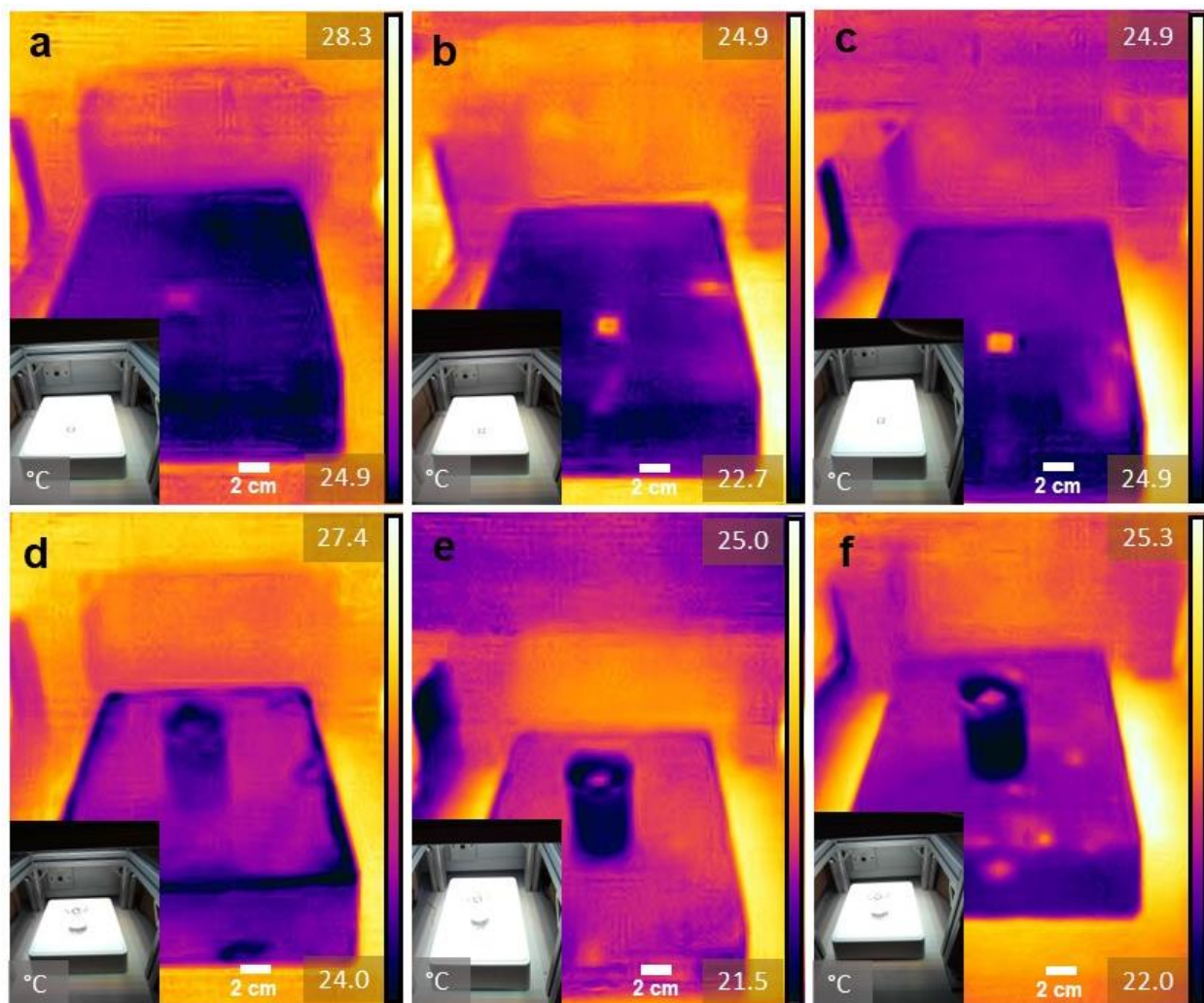


**Supplementary Figure 11 | H<sub>2</sub> evolution of SVG-PC floating directly on and suspended over seawater.** SVG-PC was not in contact with the liquid phase in the latter case. Photocatalytic experiments were performed under AM 1.5G, 22 h at room temperature. Data are presented as mean values  $\pm$  SD with  $n = 3$ .



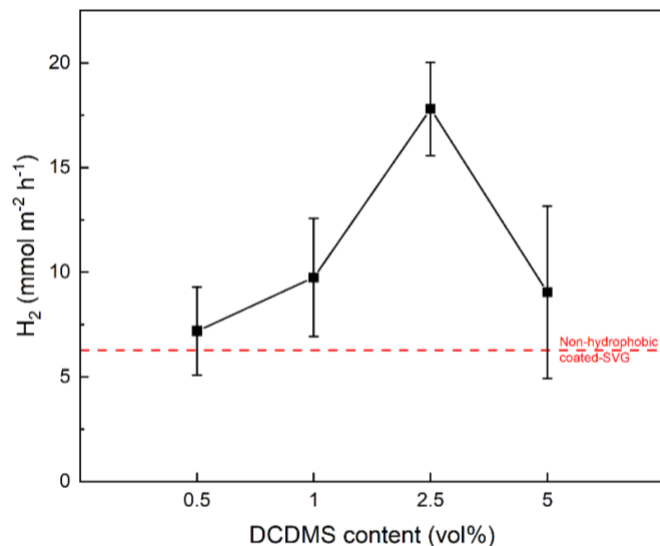


**Supplementary Figure 12 | Infrared thermal images of SVG-PC and SVG under 1 sun irradiation. a, b,** Thermal image of SVG-PC (a) and SVG (b) in air. **c, d,** Thermal image of SVG-PC (c) and SVG (d) over water. **e,** Thermal image of 25 cm<sup>2</sup> SVG-PC over water. The insets show the corresponding optical image of each sample. Bar on right of the infrared thermal images represents temperatures.

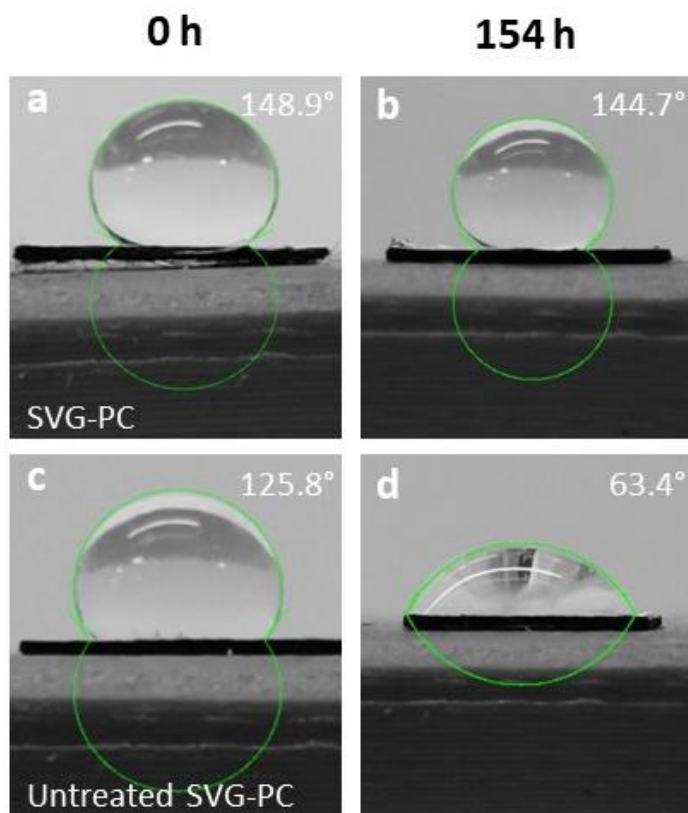


**Supplementary Figure 13 | Infrared thermal images of SVG-PC under 0.2-0.7 sun irradiation. a-c,** Thermal image of SVG-PC in air under 0.2 (a), 0.5 (b) and 0.7 (c) sun irradiation. **d-f,** Thermal image of SVG-PC floating on the surface of water under 0.2 (d), 0.5 (e) and 0.7 (f) sun irradiation. The insets show the corresponding optical image of each sample. Bar on right of the infrared thermal images represents temperatures.

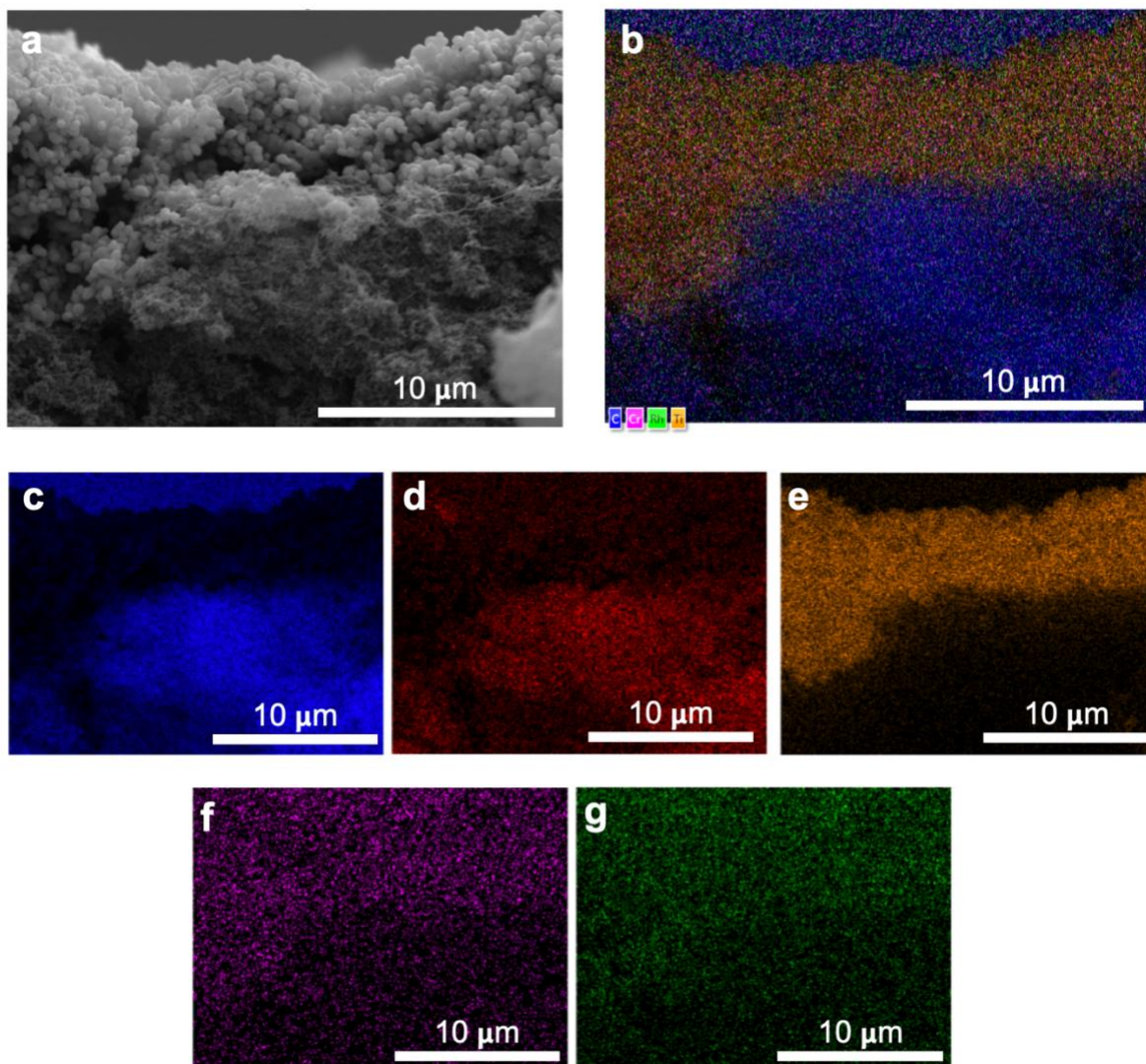




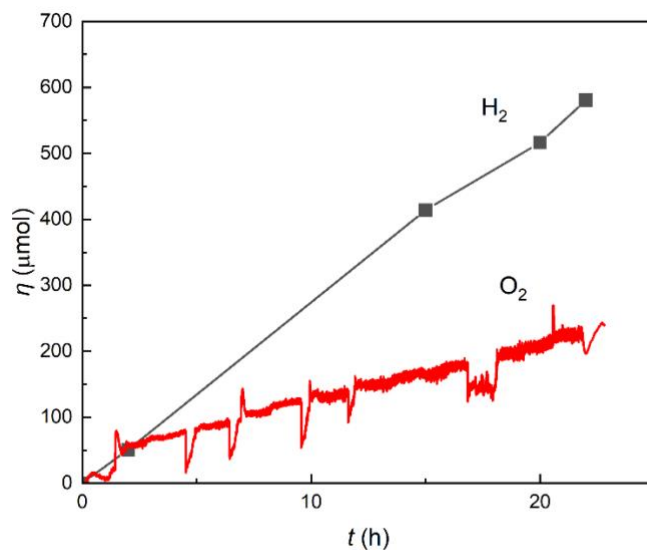
**Supplementary Figure 14 | H<sub>2</sub> evolution rate of SVG-PC fabricated on hydrophobically-treated SVG with various DCDMS concentration.** An optimum DCDMS concentration is 2.5 vol% DCDMS. Increasing the concentration of DCDMS to 5 vol% results in two times lower H<sub>2</sub> evolution rate compared to 2.5 vol% DCDMS. Reported value can be seen in Supplementary Table 17. Data are presented as mean values  $\pm$  SD with n = 3.



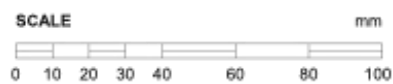
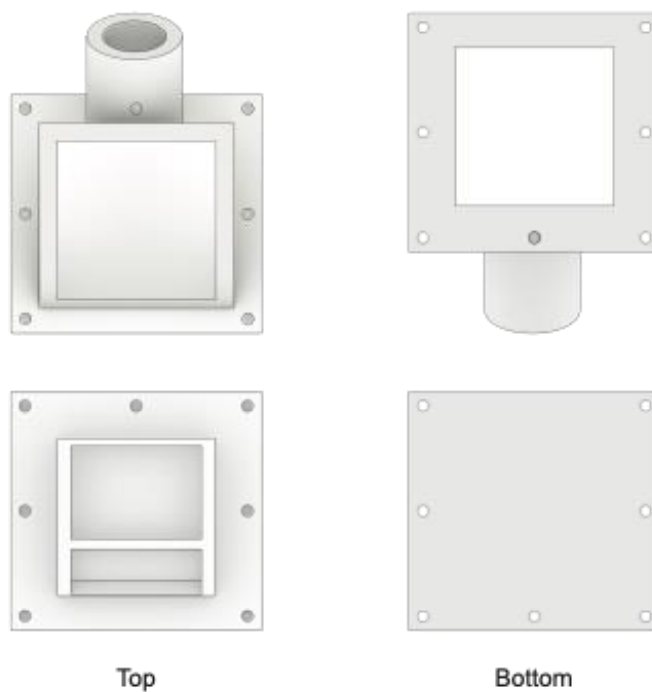
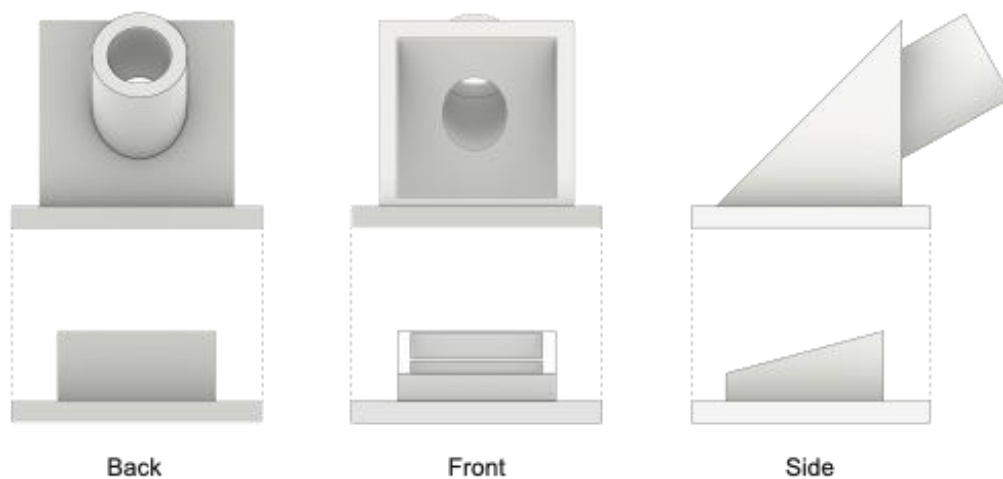
**Supplementary Figure 15 | Contact angle measurement of photocatalyst sheets.** a, b, Contact angle of SVG-PC at 0 h (a) and 154 h (b). c, d, Contact angle of untreated SVG-PC at 0 h (c) and 154 h (d).



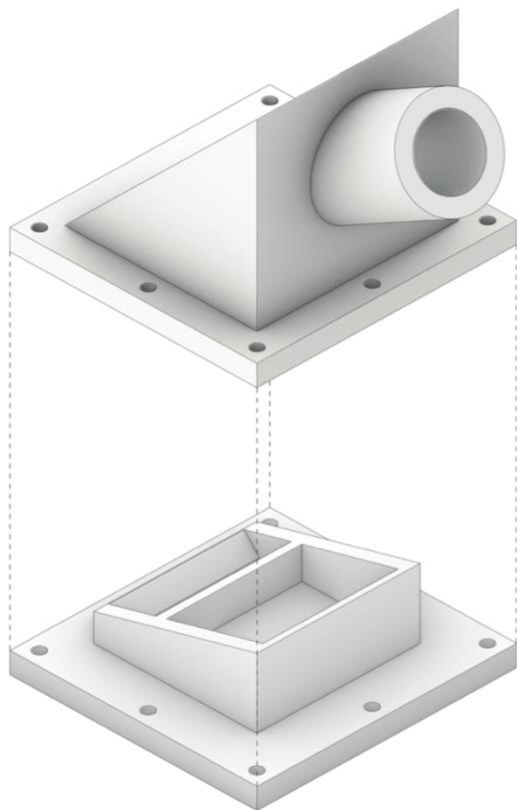
**Supplementary Figure 16 | Cross-section SEM images and energy-dispersive X-ray (EDX) elemental mapping of SVG-PC sheet after 150 h operation under 1 sun irradiation. a**, SEM image recorded at 15.0 kV beam intensity. **b-g**, Overall (b), carbon (c), fluorine (d), titanium (e), chromium (f) and rhodium (g) elemental mapping.



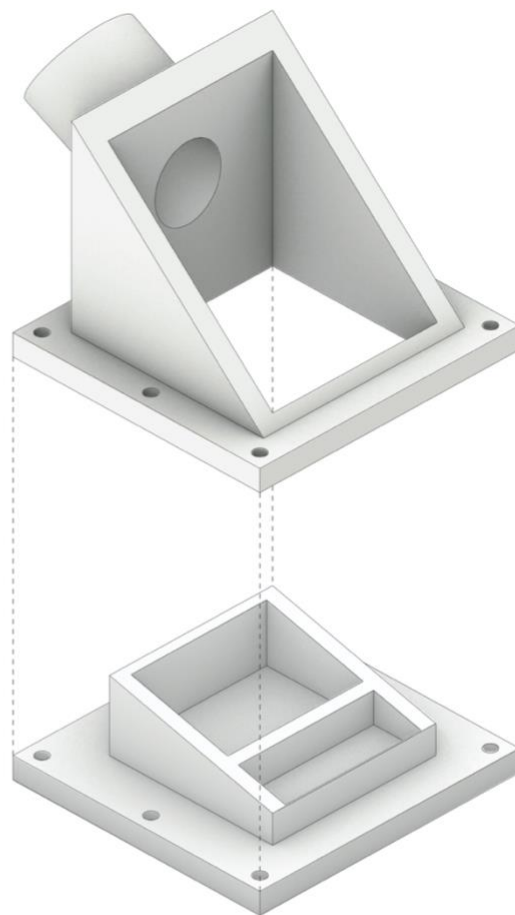
**Supplementary Figure 17 | Time course of H<sub>2</sub> and O<sub>2</sub> evolution via the water splitting reaction using 25 cm<sup>2</sup> SVG-PC over artificial seawater.** Photocatalytic measurements were performed under simulated sunlight (AM 1.5G, 100 mW cm<sup>-2</sup>). Fluctuations in the O<sub>2</sub> measurements were likely due to the formation of water droplets on the oxygen sensor probe via condensation.



**Supplementary Figure 18 | Sketches of the custom reactor used to demonstrate integrated water splitting and clean water production by hybrid photothermal-photocatalyst sheets and its components.** Diagram shows 2D projections of top, bottom and side views of the photoreactor.



Axonometric 1

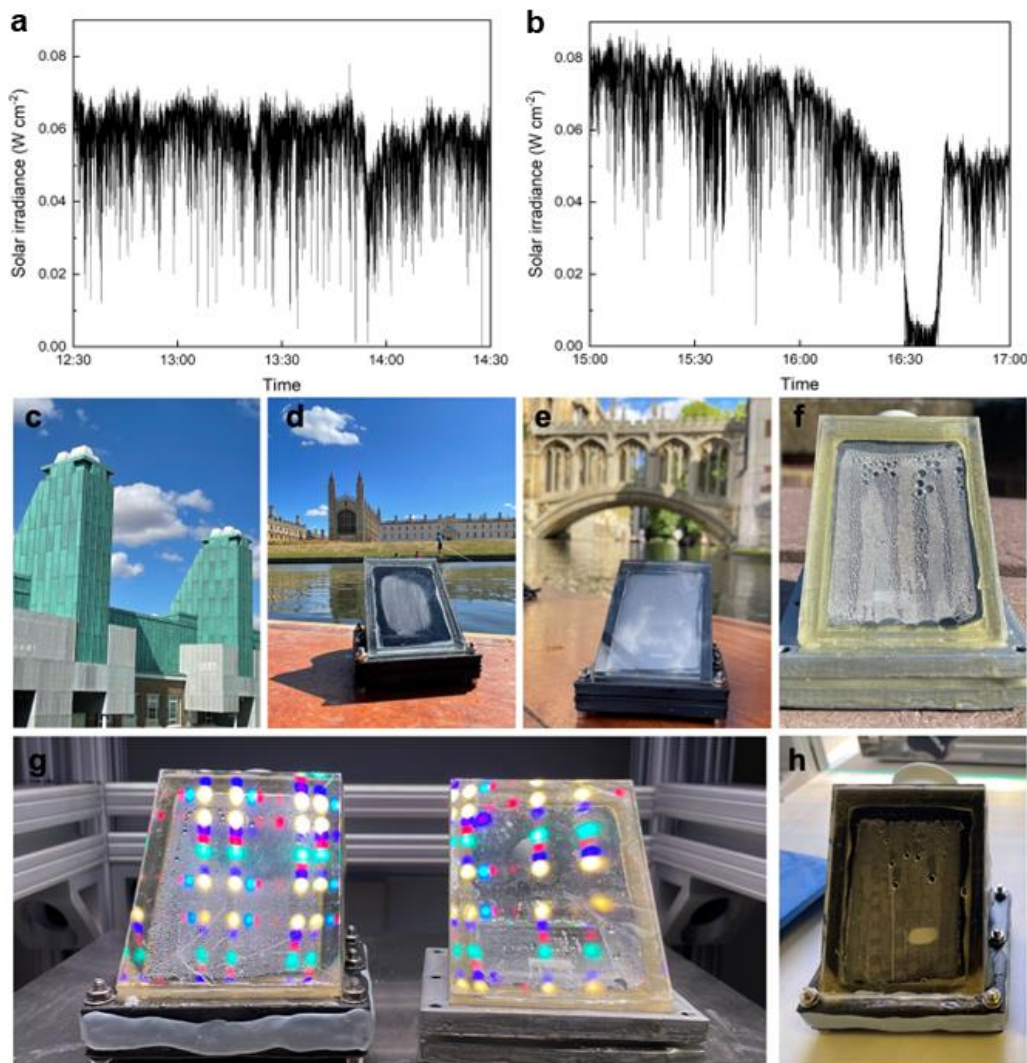


Axonometric 2

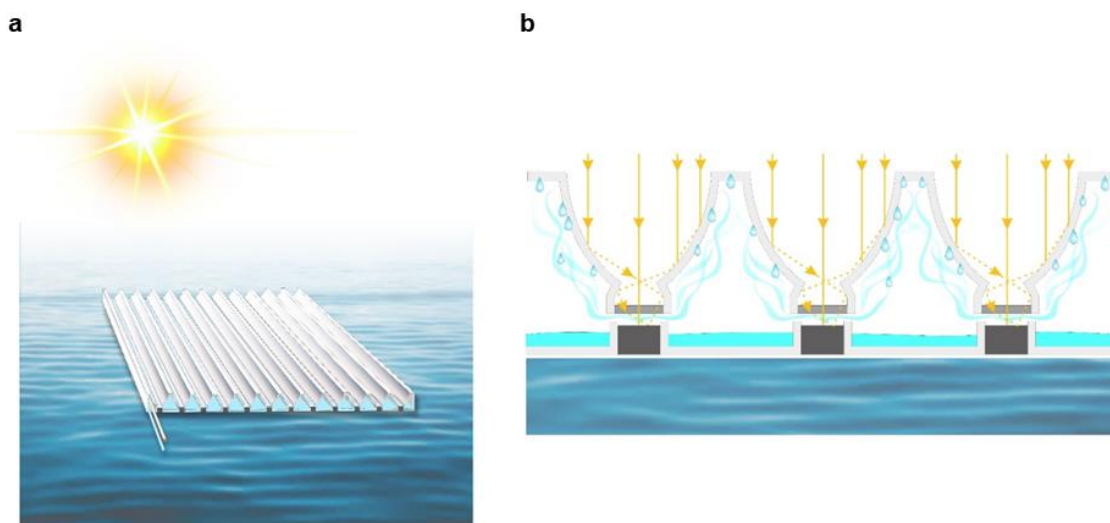
(NOT TO SCALE)

**Supplementary Figure 19 | Schematic diagram showing axonometric views of the photoreactor used to demonstrate integrated water splitting and clean water production by hybrid photothermal-photocatalyst sheets.** The 3D-printed reactor was printed using CPE+ (co-polyester) filament. UV-transmitting Plexiglass was attached to the top part of the cell using two-part epoxy.

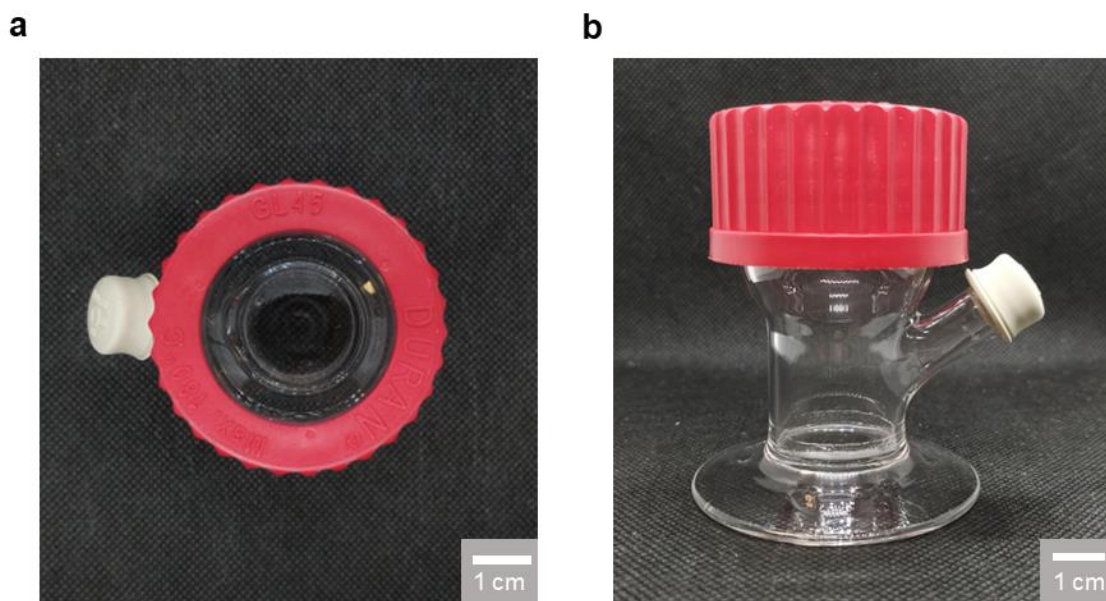




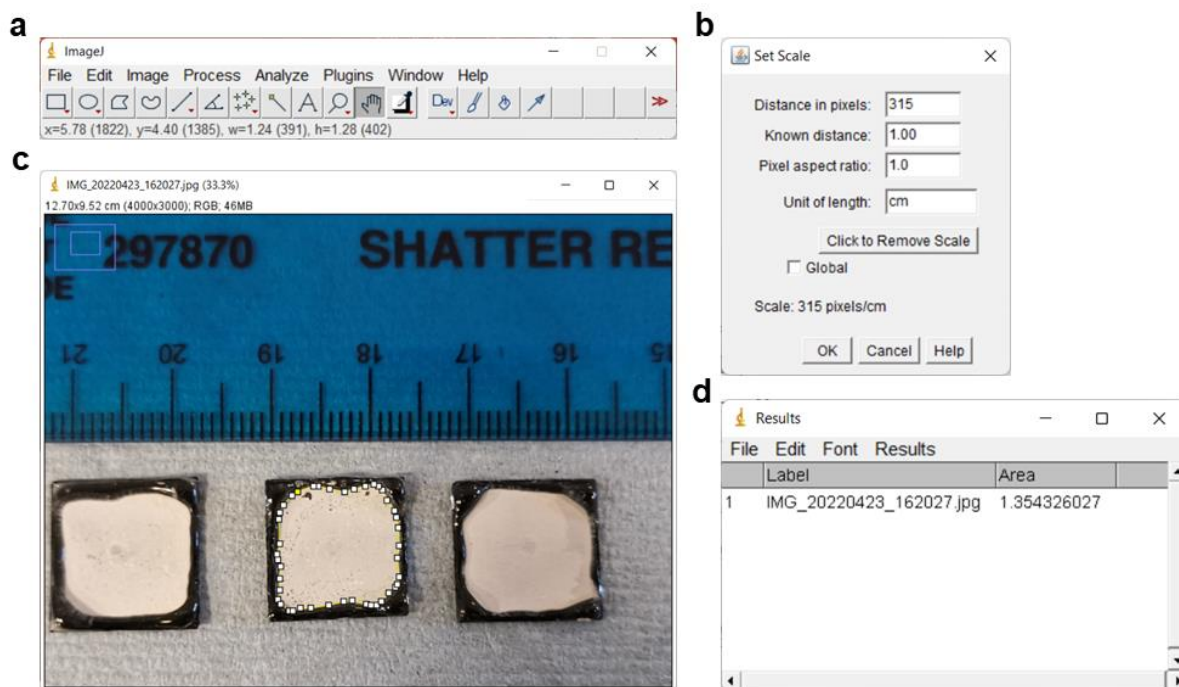
**Supplementary Figure 20 | Integrated  $\text{H}_2$  and clean water production by SVG-PC under simulated and natural sunlight using water from river Cam.** **a**, Light intensity during a 2 h test on the 6<sup>th</sup> of August 2022, between 12:30 – 14:30 (sunny, corresponding to approximately 0.6 sun,  $T \approx 21^\circ\text{C}$ ). **b**, Light intensity during a 2 h test on the 6<sup>th</sup> of August 2022, between 15:00 – 17:00 (mostly sunny with a period of overcast, corresponding to approximately 0.7 sun,  $T \approx 24^\circ\text{C}$ ). **c**, Sloped roof of the Yusuf Hamied Department of Chemistry building as inspiration for the design of the photoreactor for integrated water splitting and clean water production. **d**, **e**, Photograph of the photoreactor along the River Cam in front of King’s College Chapel (**d**) and the Bridge of Sighs, St John’s College (**e**). **f**, A closeup photo of the reactor showing condensed water droplet formed on the front window of the reactor during outdoor experiment. **g**, Indoor test conducted using a G2V Sunbrick LED Solar Simulator calibrated to match AM 1.5G irradiation. The coloured reflections correspond to the different-wavelength LEDs which are amassed to produce the AM 1.5G spectrum. **h**, Photograph of the photoreactor after conducting the photocatalytic experiment under simulated sunlight.  $\text{H}_2$  is trapped in the gas-tight headspace of the photoreactor while water vapour produced by the SVG condenses on the sloped window and accumulates to form larger droplets which then flow into a separate partition for collection.



**Supplementary Figure 21 | Proposed design of a reactor for large-scale application of the floating photocatalyst sheets with solar concentration.** **a**, 3D rendering and **b**, side-view of the reactor. The reactor can float on the surface of a body of water, such as the sea. Parabolic mirrors will concentrate sunlight onto the photocatalyst sheets. The produced water will be trapped in the reactor compartments and can be subsequently collected. The hydrogen and oxygen produced would be circulated away from the reactor headspace to reduce overpressure. The gas mixture can be transported to an on-shore gas separation unit. Gas separation could then be done via conventional membrane separation. The SVG-PC device in our proposed reactor makes a direct contact with the water supply (such as seawater and waste streams), thus omitting the need for an extra water supply and a desalination mechanism.



**Supplementary Figure 22 | Photographs of top-irradiation-type glass photoreactor used for photocatalytic reaction.** Photograph of the reactor from the top view (a) and side view (b). The optical transparent quartz window is used to allow full solar irradiation to reach the device.

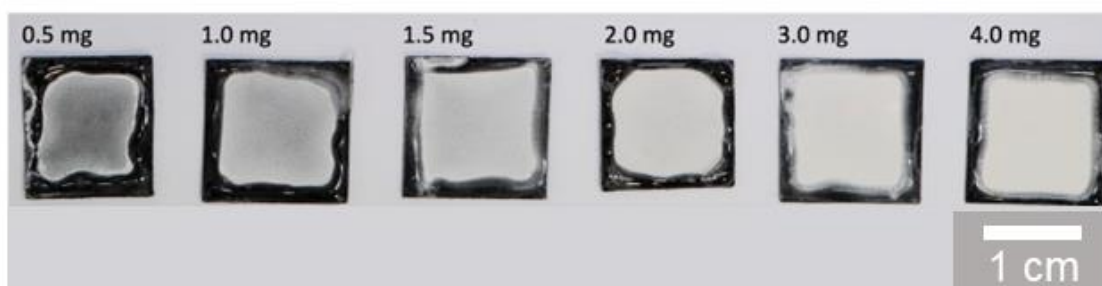


**Supplementary Figure 23 | Measurement of the photocatalyst sheet photoactive area using the ImageJ software. a,** ImageJ user interface. **b,** Calibration of the measurement tool by setting the conversion ratio of number of pixels in photograph to actual length. **c,** Highlighting the parameter of the active area of the photocatalyst sheet. **d,** Output from the software gives the area of the highlighted region.

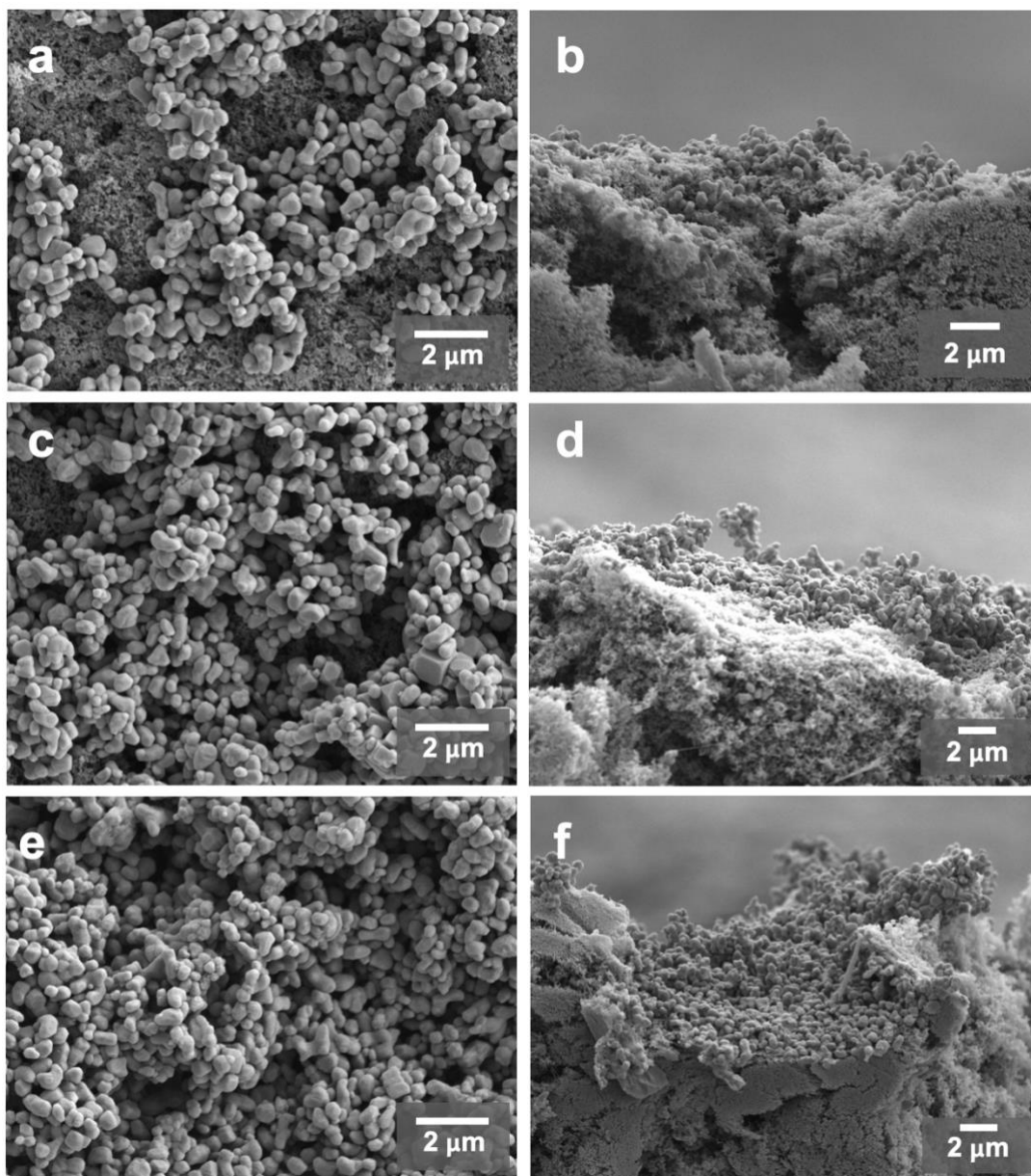




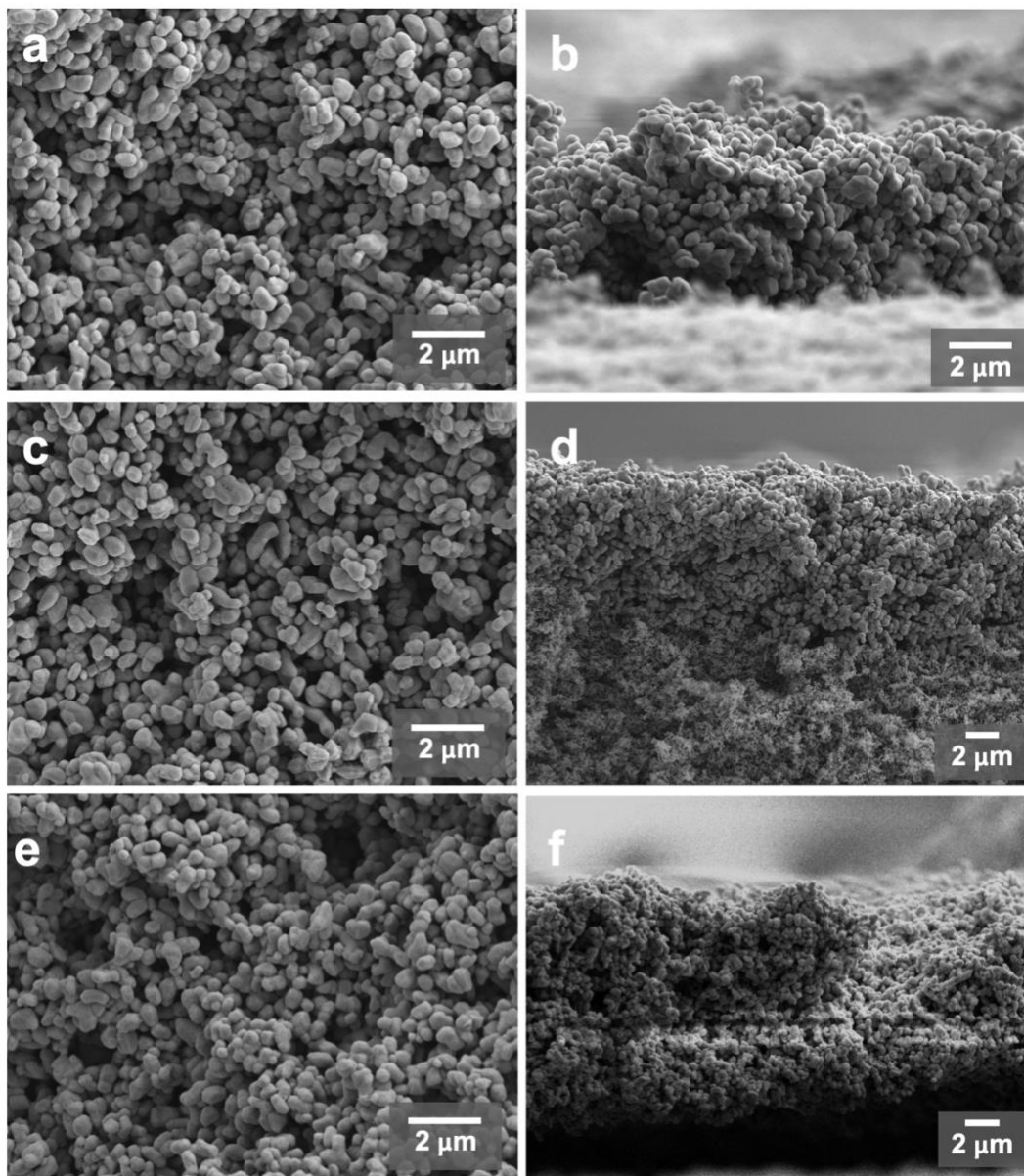
**Supplementary Figure 24 | Photographs of the custom-designed photoreactors for solar vapour characterization.** 3D-printed reactor with a dimension of  $1.5 \times 1.5 \times 5.0 \text{ cm}^3$ . The reactors were printed using polylactic acid (PLA) filament.



**Supplementary Figure 25 | Photographs of SVG-PC at different RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> loading.**



**Supplementary Figure 26 | SEM images of SVG-PC at different RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> loading. a, b, 0.5 mg cm<sup>-2</sup>-loaded SVG-PC sheet. c, d, 1.0 mg cm<sup>-2</sup>-loaded SVG-PC sheet. e, f, 1.5 mg cm<sup>-2</sup>-loaded SVG-PC sheet. a,c,e, Top views. b,d,f, Cross-section SEM images.**



**Supplementary Figure 27 | SEM images of SVG-PC at different  $\text{RhCrO}_x\text{-Al:SrTiO}_3$  loading. a, b,** Top-view (a) and Cross-section SEM image (b) of  $2.0 \text{ mg cm}^{-2}$ -loaded SVG-PC sheet. **c, d,** Top-view (a) and Cross-section SEM image (b) of  $3.0 \text{ mg cm}^{-2}$ -loaded SVG-PC sheet. **e, f,** Top-view (e) and Cross-section SEM image (f) of  $4.0 \text{ mg cm}^{-2}$ -loaded SVG-PC sheet.

**Supplementary Table 1 | ICP-OES analysis of the Rh and Cr content of photocatalyst sheets before and after 154 h of irradiation.** The photocatalysis experiments were carried out under AM 1.5G.

Sample	Element content (ppm)		Cr/Rh ratio
	Rh	Cr	
Fresh samples			
RhCrO <sub>x</sub> -Al:SrTiO <sub>3</sub> powder	0.816	0.901	1.10
SVG-PC	0.289	0.425	1.47
Samples after 154 h of operation			
Glass-PC in H <sub>2</sub> O	0.51	0.323	0.63
Glass-PC in Seawater	0.255	0.221	0.87
Untreated SVG-PC in H <sub>2</sub> O	0.408	0.255	0.63
Untreated SVG-PC in Seawater	0.153	0.238	0.66
SVG-PC-H <sub>2</sub> O	0.476	0.612	1.29
SVG-PC-Seawater	0.323	0.493	1.53

**Supplementary Table 2 | Water evaporation rate of SVG-PC with different RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> loading.** Conditions: irradiation (AM 1.5G, 1 sun, 4 h), H<sub>2</sub>O. Data are presented as mean values ± SD with n = 3.

Catalyst loading (mg)	Evaporation rate (kg m <sup>-2</sup> h <sup>-1</sup> )	Solar thermal conversion efficiency (%)
blank	0.55 ± 0.11	34.5 ± 7.1
SVG	1.07 ± 0.08	67.1 ± 5.0
0	1.07 ± 0.08	67.7 ± 5.2
0.5	0.99 ± 0.05	62.0 ± 3.1
1	0.99 ± 0.15	62.2 ± 9.4
1.5	0.93 ± 0.16	58.4 ± 10
2	0.95 ± 0.10	59.8 ± 6.2
3	0.87 ± 0.09	54.6 ± 5.5
4	0.88 ± 0.15	55.3 ± 9.4

**Supplementary Table 3 | Recent reports on solar vapour generation devices.**

Description	Optical absorption (%)	Water evaporation rate (kg m <sup>-2</sup> h <sup>-1</sup> )	Solar-thermal conversion efficiency (%)	Ref
<b>Carbonaceous materials</b>				
Water splitting photocatalyst deposited on hydrophobic-treated carbon paper	-	0.95	59.8	This work
Bare hydrophobic-treated carbon paper	-	1.07	67.1	This work
Hierarchical porous carbon supported on paper	91	1.52	81.2	<sup>19</sup>
TiN/bio-carbon foam	96	1.47	92.5	<sup>20</sup>
Graphene-nickel foam with PEDOT:PSS coating	97	1.10	73.4	<sup>21</sup>
Carbon nanotube and ultralong hydroxyapatite nanowires bilayer aerogel	96	1.34	89.4	<sup>22</sup>
Melamine-derived carbon sponges with PS thermal insulator	-	1.98	92.0	<sup>23</sup>
Carbon nanotube films	90	3.62 (5 sun irradiation)	45.5	<sup>24</sup>
<b>Plasmonic materials</b>				
Thin-film black gold membrane	91	0.67	57.0	<sup>25</sup>
PVDF membrane with Au-NP top layer	93	1.02	63.1	<sup>26</sup>
Ag/polypyrrole-modified poly(ionic liquid)s hydrogel	96	1.37	88.7	<sup>27</sup>
Pd-NP-decorated bamboo	95	0.96	71.5	<sup>28</sup>
Au nanorods with horn-like protrusions	93	2.70	79.3	<sup>29</sup>
<b>Semiconductor materials</b>				
Self-floating 3-D Ti <sub>2</sub> O <sub>3</sub> -based aerogels	95	1.31	81.7	<sup>30</sup>
Hollow multi-shelled CuO/Cu <sub>2</sub> O	82	3.20	77.0	<sup>31</sup>
CuFeSe <sub>2</sub> nanoparticle decorated wood membrane	99	1.04	67.7	<sup>32</sup>
Hierarchical copper silicone nanoscale membrane	94	0.93	58.4	<sup>33</sup>
<b>Polymer materials</b>				
Hierarchically nanostructured gels based on polyvinyl alcohol and polypyrrole	98	3.20	94.0	<sup>34</sup>
Polypyrrole-coated sodium alginate-modified poly(divinylbenzene)/polystyrene	90	1.40	87.6	<sup>35</sup>
Polyvinyl alcohol/chitosan/polypyrrole hydrogel	-	3.60	92.0	<sup>36</sup>

**Supplementary Table 4 | Recent reports on seawater splitting systems.**

Photocatalyst/Electrode	H <sub>2</sub> production rate ( $\mu\text{mol g}_{\text{cat}}^{-1} \text{h}^{-1}$ )	Efficiency	Stability (h)	Feedstock/Electrolyte	Sacrificial agent	Ref
<b>Photocatalysis systems</b>						
RhCrO <sub>x</sub> -Al: SrTiO <sub>3</sub> (floating)	1054	0.11% STH	150	Artificial seawater	-	This work
RhCrO <sub>x</sub> -Al: SrTiO <sub>3</sub> (submerged)	355	0.04% STH	66	Artificial seawater	-	This work
Pt/TiO <sub>2</sub> nanoparticles	1476	0.002% STH*	40	Natural Seawater	-	37
C-TiO <sub>2</sub> /WS <sub>2</sub> / g-C <sub>3</sub> N <sub>4</sub>	1199	5.06 AQE at 420 nm	25	Natural Seawater	Triethanolamine.	38
Pt/Hollow tubular g-C <sub>3</sub> N <sub>4</sub>	6782	6.9% AQE at 420 nm	8	3.5% NaCl solution	Triethanolamine.	39
Pt-loaded conjugated molecule PorFN	10800	1.2 h <sup>-1</sup> TOF	6	2.8% NaCl solution	-	40
Carbon dots/CdS nanosheets	4693	12% AQE at 420 nm	100	Natural seawater	Lactic acid.	41
CoP/P-doped Zn <sub>0.5</sub> Cd <sub>0.5</sub> S	3956	-	15	3.2% NaCl solution	Ascorbic acid.	42
Ag/TiO <sub>2</sub> /SiO <sub>2</sub>	816	-	10	3.5% NaCl solution	Glycerol.	43
Pt/P-doped g-C <sub>3</sub> N <sub>4</sub>	11900	12.1% AQE at 420 nm	16	Natural seawater	Triethanolamine.	44
Rh <sub>2-y</sub> Cr <sub>y</sub> O <sub>3</sub> loaded (Ga <sub>1-x</sub> Zn <sub>x</sub> )(N <sub>1-x</sub> O <sub>x</sub> )	1000	-	5	Artificial seawater	-	45
ZnO(nanorod)/Pt/Cd <sub>0.8</sub> Zn <sub>0.2</sub> S	23700	-	-	Natural seawater	Benzoyl alcohol/acetic acid.	46
<b>Photoelectrochemical systems</b>						
Bi-BiOI – TiO <sub>2</sub> nanotube arrays	-	2.21% STH	16	0.1 M Na <sub>2</sub> S + 0.2 M Na <sub>2</sub> SO <sub>3</sub> , 3.5 % NaCl solution.	-	47
RhCrO <sub>x</sub> /p-GaN/InGaN/CoO <sub>x</sub>	6.15 × 10 <sup>6</sup>	1.9% STH	3	Artificial seawater	-	48
Fe <sub>2</sub> O <sub>3</sub> /TiO <sub>2</sub> – Pt	-	0.49% STH	72	1.0 M NaOH, 3.5% NaCl solution.	-	49
RhO <sub>2</sub> /BiVO <sub>4</sub> :Mo – Pt	-	0.6% STH	4.5	Natural seawater.	-	50
n-ZnSe/n-Ag <sub>8</sub> SnS <sub>6</sub> – Pt	-	0.74% STH	0.8	0.5 M NaCl solution.	-	51
<b>Photovoltaic-electrochemical systems</b>						
Si SC + NiFe/ NiS <sub>x</sub> -Ni – Ni-NiO-Cr <sub>2</sub> O <sub>3</sub>	-	11.9% STH	1000	1.0 M KOH with 0.5 M NaCl solution.	-	52
InGaP/GaAs/Ge + MHCM-z-BCC/NiMoS	-	17.9% STH	100	Neutral-buffered seawater.	-	53
Si SC + NiFeOOH – (Co,Fe)PO <sub>4</sub>	-	12.8% STH	50	1.0 M KOH, natural seawater.	-	54
Si SC NiCoS – NiMoS	-	15.13% STH	14	1.0 M KOH, natural seawater.	-	55
Si SC Karst Ni foam – karst Ni foam	-	16.5% STH	24	1.0 M phosphate-buffered solution, natural seawater.	-	56

\* Calculated assuming AM1.5G irradiation was used.

**Supplementary Table 5 | Oxygen characterization for SVG-PC under different conditions.** The experiments were carried out in a N<sub>2</sub>-filled glovebox to avoid any O<sub>2</sub> leakage from the surrounding to the reactor. O<sub>2</sub> evolution was monitored by a NeoFox-GT fluorometer and FospoR-R fluorescence oxygen sensor probe from Ocean Optics and H<sub>2</sub> was monitored using GC. Note that O<sub>2</sub> measurements were performed under a different light source with modifications to the experimental setup, leading to slight differences in performance between O<sub>2</sub> measurement experiments and the other experiments. n.d. – not detected (below the instrument detection limit). Data for SVG-PC over H<sub>2</sub>O and seawater are presented as mean values ± SD with n = 2.

Sample	Feedstock	nH <sub>2</sub> (μmol cm <sup>-2</sup> )	nO <sub>2</sub> (μmol cm <sup>-2</sup> )
Glass-PC	H <sub>2</sub> O	39.1	10.5
	Seawater	9.9	n.d.
Untreated SVG-PC	H <sub>2</sub> O	38.2	23.1
	Seawater	16.8	12.5
	H <sub>2</sub> O	44.1 ± 8.3	25.6 ± 3.3
	Seawater	43.5 ± 4.3	20.6 ± 2.6
SVG-PC	IPA	33.6	14.1
	Turbid	21.5	9.3
	River Cam	33.7	13.4

**Supplementary Table 6 | Sample time course of H<sub>2</sub> evolution using SVG-PC floating on pure water and seawater.** Conditions: 2.0 mg RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> deposited on hydrophobic-treated SVG, irradiation (AM 1.5G, 1 sun, 22 h), H<sub>2</sub>O or artificial seawater. Data are presented as mean values ± SD with n = 3.

Feedstock	Time (h)	H <sub>2</sub> (μmol cm <sup>-2</sup> )
H <sub>2</sub> O	2	2.56 ± 0.09
	4	7.30 ± 0.32
	8	15.8 ± 0.65
	22	46.7 ± 9.3
Seawater	2	3.49 ± 0.53
	4	7.00 ± 0.87
	8	14.0 ± 0.82
	22	39.1 ± 4.89

**Supplementary Table 7 | H<sub>2</sub> evolution rate of SVG-PC under UV and Vis-NIR light.** Photocatalytic measurements were performed over pure water for 22 h. n.d. – not detected. Data are presented as mean values  $\pm$  SD with n = 3.

Light condition	H <sub>2</sub> (mmol m <sup>-2</sup> h <sup>-1</sup> )	STH (%)
UV only	13.0 $\pm$ 0.65	0.08 $\pm$ 0.004
Vis-NIR only	n.d.	n.d.

**Supplementary Table 8 | Water evaporation rate of SVG-PC and SVG under UV irradiation.** Conditions: UV irradiation, 4 h, H<sub>2</sub>O. Data are presented as mean values  $\pm$  SD with n = 3.

Sample (mg)	Evaporation rate (kg m <sup>-2</sup> h <sup>-1</sup> )
blank	0.29 $\pm$ 0.02
SVG	0.56 $\pm$ 0.07
SVG-PC	0.59 $\pm$ 0.07

**Supplementary Table 9 | H<sub>2</sub> evolution of SVG-PC floating directly on and suspended over seawater.** Photocatalytic experiments were performed under AM 1.5G, 22 h, at room temperature. Data are presented as mean values  $\pm$  SD with n = 3.

Light condition	H <sub>2</sub> (mmol m <sup>-2</sup> h <sup>-1</sup> )	STH (%)
Floating	17.8 $\pm$ 2.2	0.11 $\pm$ 0.02
Suspended	2.03 $\pm$ 0.56	0.009 $\pm$ 0.002



**Supplementary Table 10 | Photocatalytic performance of Glass-PC, Untreated SVG-PV and SVG-PC in various wastewater sources.** Conditions: 2.0 mg RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> deposited on glass, SVG, hydrophobic-treated SVG, or suspended directly in liquid, irradiation (AM 1.5G, 1 sun, 22 h), H<sub>2</sub>O or artificial seawater. Data are presented as mean values ± SD with n = 3.

Sample	Feedstock	H <sub>2</sub> (mmol m <sup>-2</sup> h <sup>-1</sup> )	STH (%)
Glass-PC	H <sub>2</sub> O	25.9 ± 3.80	0.17 ± 0.02
	Seawater	6.36 ± 0.30	0.04 ± 0.002
Untreated SVG-PC	H <sub>2</sub> O	17.6 ± 1.80	0.12 ± 0.01
	Seawater	6.28 ± 0.93	0.04 ± 0.01
SVG-PC	H <sub>2</sub> O	21.2 ± 4.20	0.13 ± 0.03
	Seawater	17.8 ± 2.20	0.11 ± 0.02
	River water	19.8 ± 1.50	0.13 ± 0.01
	Turbid waste	18.9 ± 0.46	0.12 ± 0.003
Suspended-PC	H <sub>2</sub> O	20.4 ± 4.90	0.13 ± 0.03

**Supplementary Table 11 | ICP-OES analysis showing content of various elements in distillate produced from various wastewater sources.**

Water source	Element content (ppm)											
	Raw						Purified					
	Na	K	Ca	Mg	S	Si	Na	K	Ca	Mg	S	Si
Seawater	30816	952	1304	2544	1462	3172	9.11	0.09	n.d.	n.d.	0.14	9.41
River water	77.30	5.68	142.78	5.25	20.53	53.00	8.78	0.05	n.d.	n.d.	0.04	8.60
Turbid waste	21028	4048	462	80	380	5064	9.07	0.09	0.04	n.d.	0.12	9.66

**Supplementary Table 12 | Photocatalytic performance of SVG-PC under different light intensities.** Conditions: 2.0 mg RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> deposited on hydrophobic-treated SVG, irradiation (22 h), artificial seawater. Data are presented as mean values  $\pm$  SD with n = 3.

Light intensity (sun)	H <sub>2</sub> (mmol m <sup>-2</sup> h <sup>-1</sup> )	STH (%)	Evaporation rate (kg m <sup>-2</sup> h <sup>-1</sup> )
1.5	32.6 $\pm$ 2.49	0.14 $\pm$ 0.01	1.58 $\pm$ 0.12
1	17.8 $\pm$ 2.20	0.11 $\pm$ 0.02	0.95 $\pm$ 0.10
0.7	9.00 $\pm$ 0.85	0.08 $\pm$ 0.01	0.81 $\pm$ 0.13
0.5	5.31 $\pm$ 0.53	0.07 $\pm$ 0.01	0.62 $\pm$ 0.03
0.2	1.71 $\pm$ 0.13	0.06 $\pm$ 0.004	0.55 $\pm$ 0.02

**Supplementary Table 13 | Long-term photocatalytic performance of Glass-PC, untreated SVG-PC and SVG-PC in pure water and simulated seawater.** Conditions: 2.0 mg RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> deposited on glass, SVG or hydrophobic-treated SVG, irradiation (AM 1.5G, 1 sun, 22 h per cycle), reactors re-purged with N<sub>2</sub> containing 2% CH<sub>4</sub> between cycles.

Sample	Feedstock	H <sub>2</sub> ( $\mu$ mol)						
		Cycle 1	Cycle 2	Cycle 3	Cycle 4	Cycle 5	Cycle 6	Cycle 7
Glass-PC	H <sub>2</sub> O	73.10	61.22	45.06	43.69	42.50	48.96	36.75
	Seawater	13.74	10.54	11.59	9.56	9.60	8.61	10.47
Untreated SVG-PC	H <sub>2</sub> O	50.85	53.45	53.29	58.34	59.57	47.85	45.37
	Seawater	8.08	12.83	1622	7.54	7.17	6.77	5.48
SVG-PC	H <sub>2</sub> O	47.68	50.09	54.66	53.34	56.52	56.99	51.41
	Seawater	47.63	43.80	52.65	48.13	40.98	41.30	37.87

**Supplementary Table 14 | Integrated H<sub>2</sub> and clean water production rate of SVG-PC under AM 1.5G irradiation and natural sunlight.** Conditions: 2.0 mg RhCrO<sub>x</sub>-SrTiO<sub>3</sub>:Al deposited on hydrophobic-treated SVG, river water. The values are the average of duplicate experiments. Data are presented as mean values ± SD with n = 2.

Light conditions	H <sub>2</sub> (mmol m <sup>-2</sup> h <sup>-1</sup> )	Evaporation rate (kg m <sup>-2</sup> h <sup>-1</sup> )
AM 1.5G	16.1 ± 3.64	0.94 ± 0.12
Natural sunlight	7.82 ± 1.52	0.71 ± 0.12

**Supplementary Table 15 | Techno-economic analysis of floating photothermal-photocatalyst sheet and particulate photocatalyst water splitting panel systems.**

Floating photothermal- photocatalyst sheets <sup>a</sup>	\$	Particulate photocatalyst water splitting panels <sup>a</sup>	\$
<b>Expenditure</b>			
<b>Capital</b>			
Reactor subassembly <sup>9</sup>	6,022,872	Reactor subassembly	6,022,872
Solar vapour generator <sup>57</sup>	104,915	Glass panels <sup>58</sup>	28,000
Gas separation and storage <sup>13</sup>	1,142,860	Gas separation and storage	1,142,860
Piping <sup>9</sup>	104,861	Piping	104,861
Control system <sup>9</sup>	319,862	Control system	319,862
Land <sup>14</sup>	94,055	Land	457,107
<b>Subtotal</b>	<b>7,789,425</b>		<b>8,075,562</b>
<b>Operation (over 20-year span)</b>			
Operating labour <sup>59</sup>	1,051,200	Operating labour	1,051,200
Power usage <sup>12</sup>	2,106,636	Power usage	2,106,636
Maintenance and repair <sup>60</sup>	389,471	Maintenance and repair	403,778
<b>Subtotal</b>	<b>3,447,307</b>		<b>3,561,614</b>
<b>Consumables (over 20-year span)</b>			
Photocatalyst <sup>b</sup> <sup>61-63</sup>	49,990	Photocatalyst	19,995
		Pure water <sup>64</sup>	6,307,200
<b>Consumables subtotal</b>	<b>49,990</b>		<b>6,327,195</b>
<b>Expenditure subtotal</b>	<b>11,286,722</b>		<b>17,964,371</b>
<b>Revenue (over 20-year span)</b>			
H <sub>2</sub> <sup>c</sup>	14,235,000		14,235,000
<b>Revenue subtotal</b>	<b>14,235,000</b>		<b>14,235,000</b>
<b>Net</b>	<b>2,948,278</b>		<b>-3,729,371</b>

<sup>a</sup> STH of 10%, capacity of 1 tonne per day of H<sub>2</sub>, average solar insolation of 0.24 kW m<sup>-2</sup>, facility lifetime of 20 years.<sup>9,11,65</sup>

<sup>b</sup> CoP-modified graphitic carbon nitride was used as a model photocatalyst.<sup>15-17</sup>

<sup>c</sup> Estimated from market price of H<sub>2</sub> and tax credits available for green H<sub>2</sub> production.<sup>66</sup>

**Supplementary Table 16 | Photocatalytic performance of SVG-PC with different RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> loading for overall solar water splitting.** Conditions: RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> deposited on untreated SVG, irradiation (AM 1.5G, 1 sun, 22 h), H<sub>2</sub>O. Data are presented as mean values ± SD with n = 3.

Catalyst loading (mg)	H <sub>2</sub> (mmol g <sub>cat</sub> <sup>-2</sup> h <sup>-1</sup> )	H <sub>2</sub> (mmol m <sup>-2</sup> h <sup>-1</sup> )	STH (%)
0	n.d	n.d	-
0.5	1.14 ± 0.29	5.22 ± 1.20	0.034 ± 0.01
1	1.40 ± 0.12	11.1 ± 1700	0.073 ± 0.01
1.5	1.19 ± 0.10	14.3 ± 1.90	0.094 ± 0.01
2	1.20 ± 0.95	17.6 ± 1.80	0.11 ± 0.01
3	0.78 ± 0.63	18.9 ± 4.10	0.12 ± 0.03
4	0.67 ± 0.06	20.6 ± 3.70	0.13 ± 0.02

**Supplementary Table 17 | Photocatalytic performance of SVG-PC after treatment with DCDMS solution with different silane content.** Conditions: 2.0 mg RhCrO<sub>x</sub>-Al:SrTiO<sub>3</sub> deposited on SVG, irradiation (AM 1.5G, 1 sun, 22 h), artificial seawater. Data are presented as mean values ± SD with n = 3.

Silane content (%)	H <sub>2</sub> (mmol m <sup>-2</sup> h <sup>-1</sup> )	STH (%)
0	6.28 ± 0.93	0.04 ± 0.01
0.5	7.19 ± 2.10	0.05 ± 0.01
1.0	9.75 ± 2.80	0.06 ± 0.02
2.5	17.8 ± 2.20	0.11 ± 0.02
5.0	9.04 ± 4.10	0.06 ± 0.03

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End of Supporting Information